



SÁEZ JIMÉNEZ, CRISTINA

Full Professor

Universidad de Castilla-La Mancha



DISMANTLING STRATEGIES FOR HIGHLY HCH-POLLUTED LANDFILL LEACHATE POND USING ELECTROCHEMICALLY ASSITED TECHNOLOGY

Isidro, J., Fernández-Cascán, J., Guadaño, J., Sáez, C., Rodrigo, M.A



Introduction



Old landfill
leachate pond



Sardas landfill



Sabiñánigo
reservoir

Old landfill
leachate pond





Old landfill leachate pond:

- **HPDE sheet and dimension of 50x25 m²**
- **Thickness of more than 1 m of sludge (saturated and without compacting)**
- **Heterogeneous HCH contamination. From few mg/kg to dozen g/kg**
- **It is currently collecting runoff and leachate drained in the ditch and leachate pumped from boreholes, which includes contributions of DNAPL microdroplets**





CRITICAL dismantling

**Risk of affecting
groundwater and
Sabiñánigo reservoir**



CRITICAL dismantling

- ✓ to not damage the sheet of the pond
- ✓ To avoid leachate infiltration
- ✓ to not affect quality of surface water
- ✓ To guarantee the safety and health of the operators





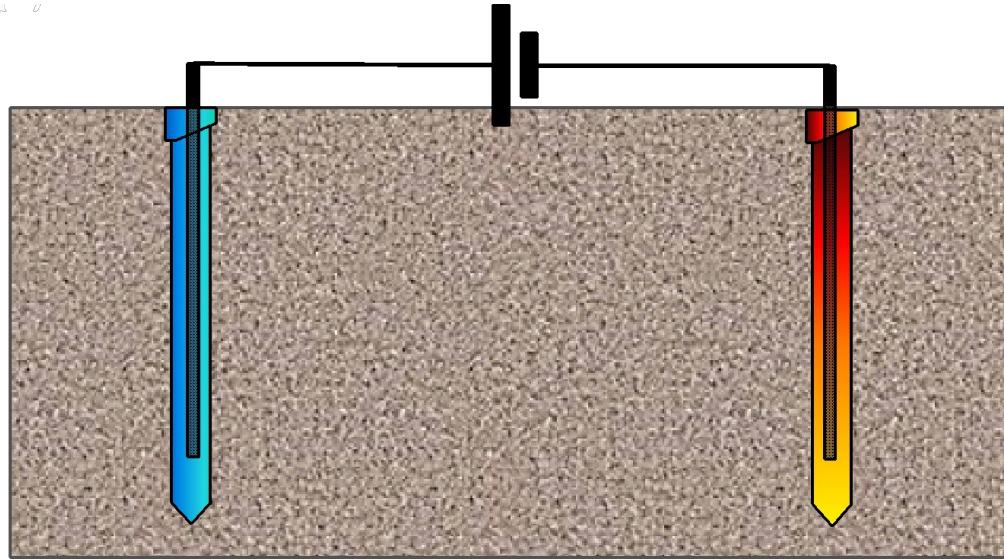
Sludge characteristics:

- ✓ black color, with gray tones on the surface by oxidation
- ✓ very plastic, adherent and difficult to handle.





What happens when we apply an electric field to electrodes placed in the sludge?

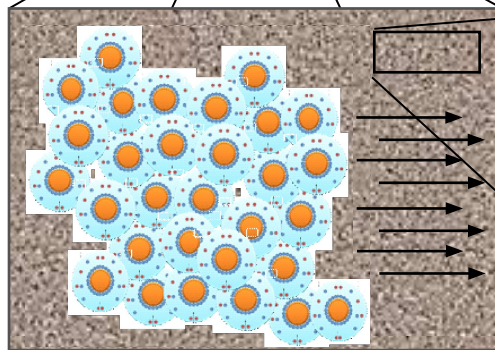
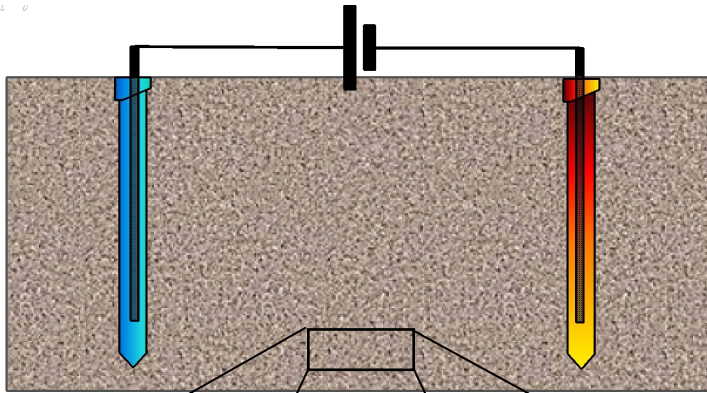


Includes ***different processes*** that take part in a soil:

- ☐ Physical processes (heating)
- ☐ Chemical processes (ionic exchange, precipitations, etc.)
- ☐ Electrochemical processes (water oxidation and reduction)
- ☐ Electrokinetic processes (electrosmosis, electrophoresis and electromigration)

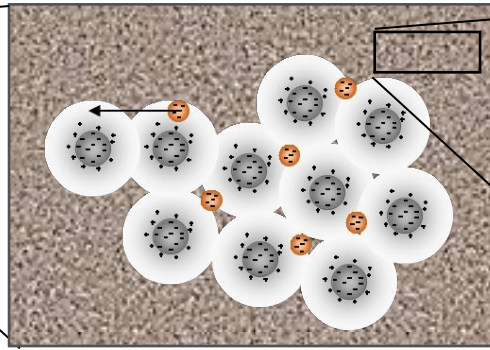
Electrokinetic processes

Includes ***different processes*** that take part in a soil as a result of the application of an electric field.



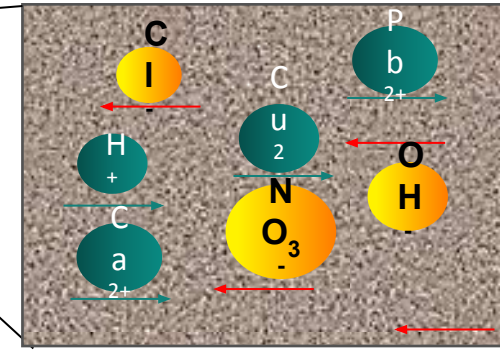
MACROSCOPIC LEVEL

Electro-osmosis
movement of the water into the soil through the application of electric field.



MICROSCOPIC LEVEL

Electrophoresis
movement of the charged particles into the soil through the application of electric field.

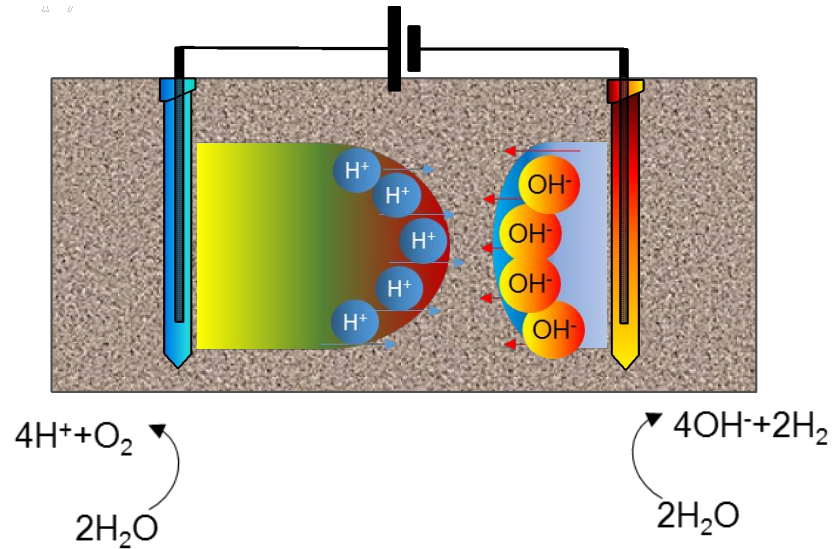


MOLECULAR LEVEL

Electromigration
movement of the ions into the soil through the application of electric field.

Electrolysis

Water oxidation on the anodic surface
Water reduction on the cathodic surface

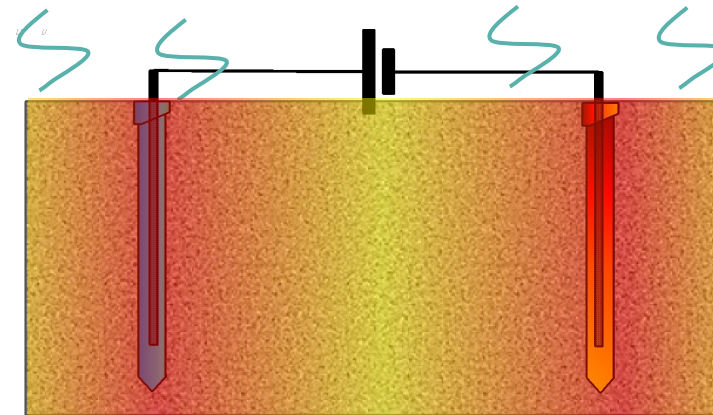


Influences on:

- ☐ Different species precipitation / redissolution
- ☐ Fixation or liberation of species by ionic exchange
- ☐ Microbial viability

Soil electrical heating

Temperature increase that occurs in the soil due to the ohmic drop generated by the **high electrical resistance** of the soil.



Influences on:

- ☐ Viscosity changes in liquids contained in the soil
- ☐ Pollutants volatilization
- ☐ Water evaporation



Objectives

TO DISMANTLE HIGHLY HCH-POLLUTED LANDFILL LEACHATE POND USING ELECTROCHEMICALLY ASSISTED TECHNOLOGY

The ideal conditions for dismantling the pond would be:

- **To reach a level of dryness in the sludge that would allow its mechanical handling without risk.**
- **To minimize the atmospheric emissions.**
- **To minimize the need for necessary infrastructure and equipment, as well as subsequent treatments for conditioning, transfer, or decontamination**

Partial technical objectives

To determine the **mobility of pollutants** in the sludge under the action of **electric field**.

To evaluate the **dewatering** of the sludge by the action of the **electric field**.

To study the **treatment of water** mobilized and recovered from the treatment by **electrochemical** technologies.

To evaluate the implementation of **GAC column** to retain **organics** transfer to the **atmosphere**

To **implement the technology** in real scale



Results



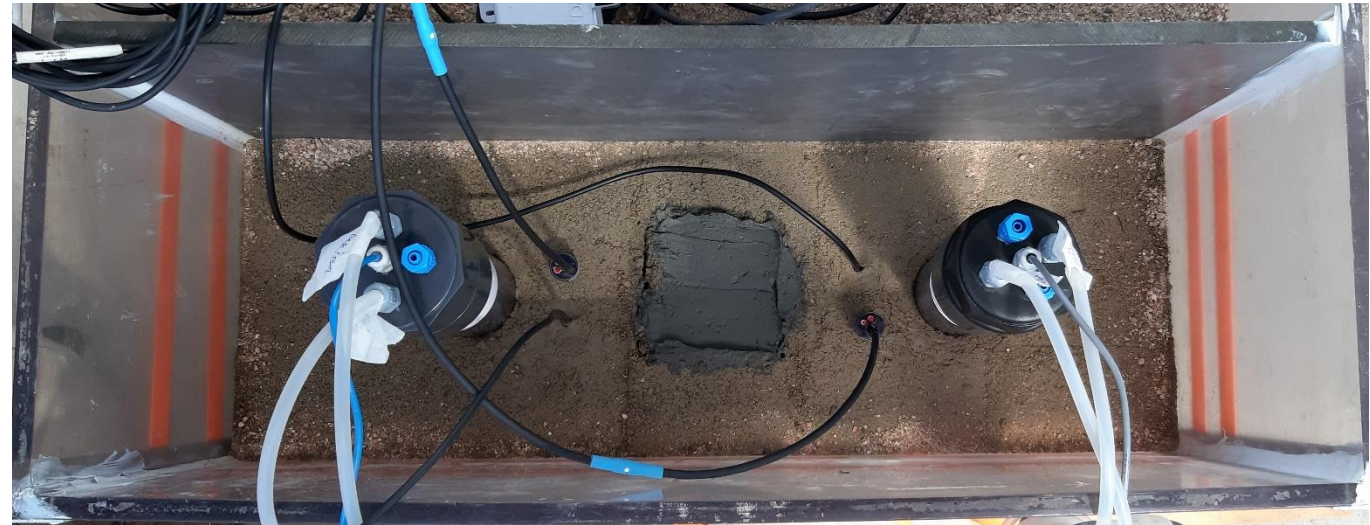
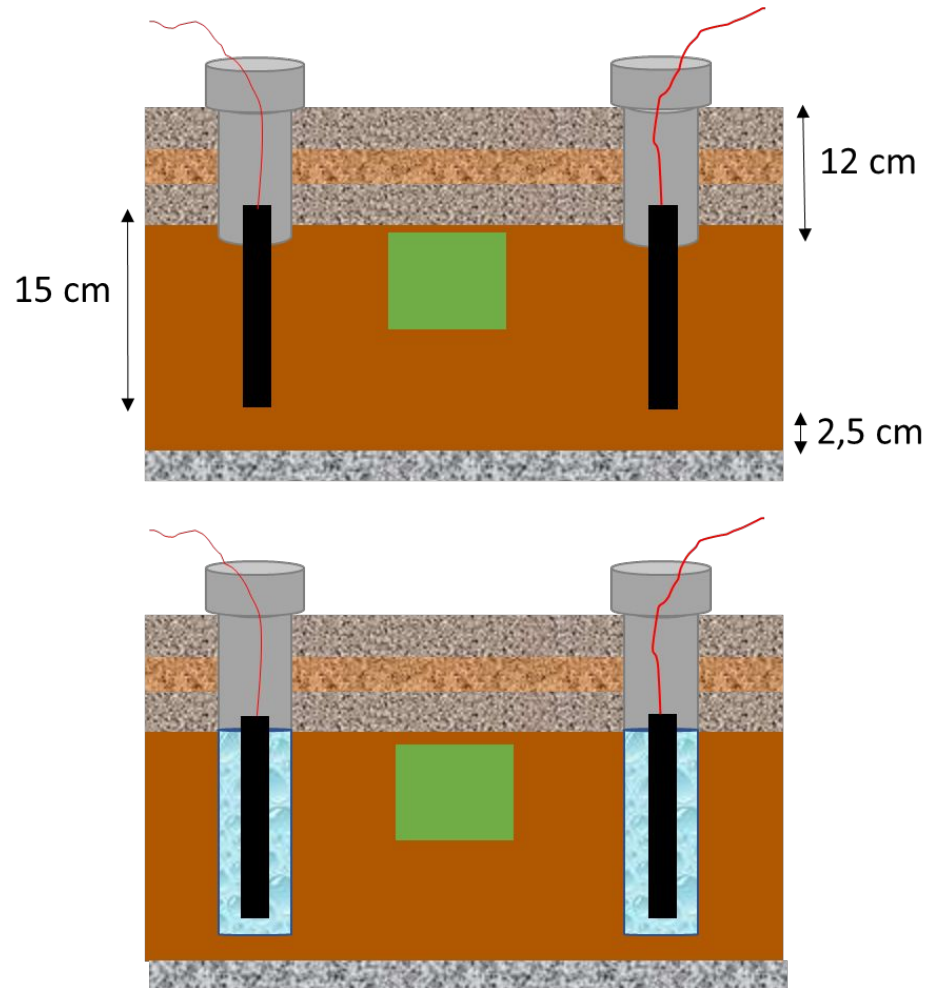
1 Study of
mobilization

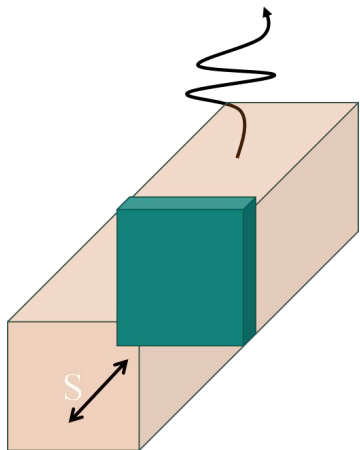
2 EK treatment
and dewatering
of the sludge at
bench scale

3 Electrochemical
treatment of
liquid streams

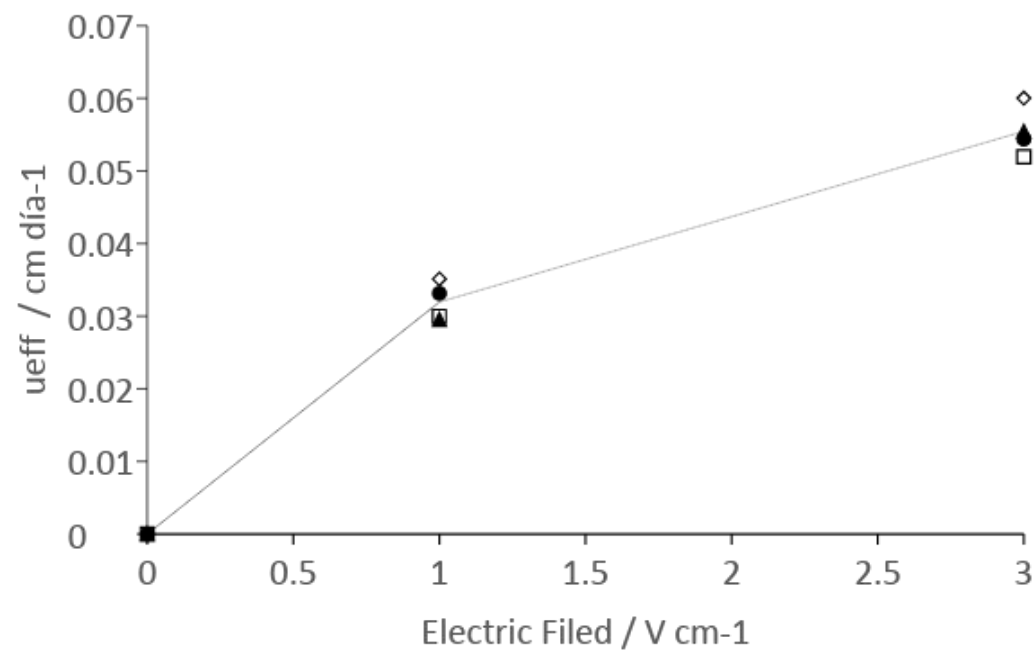
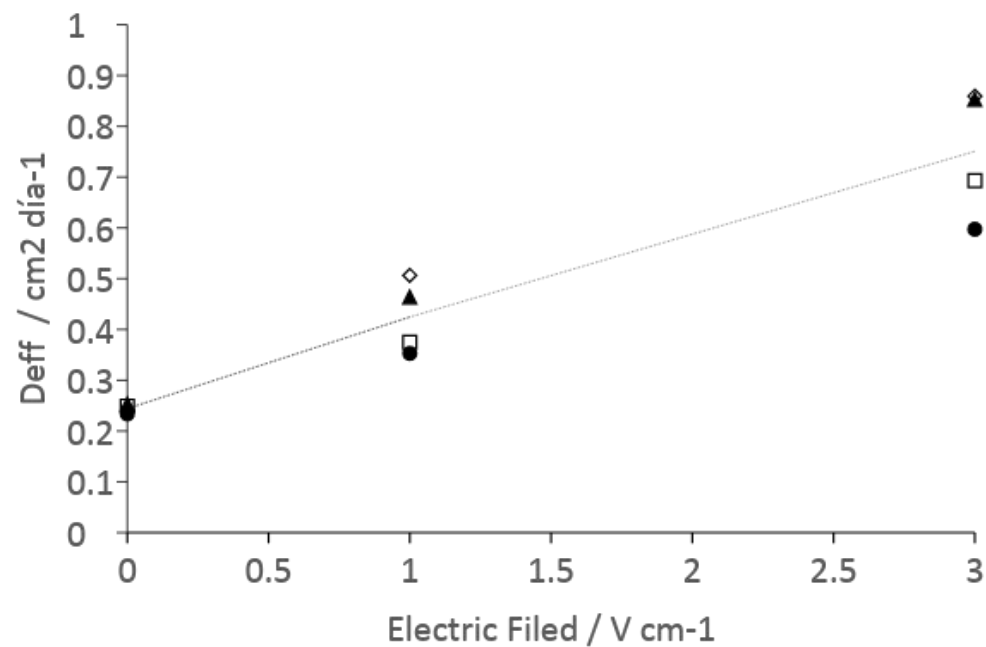
4 Field
application

Characterization of sludge water and contaminant mobility under the action of the electric field during the first electrochemically assisted stage. Stage1.

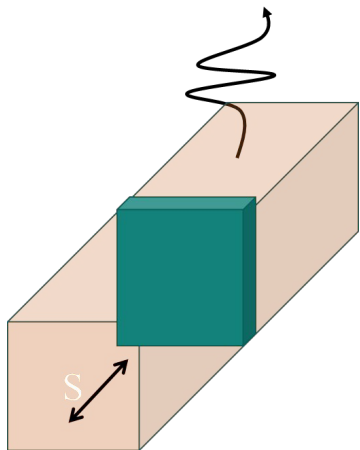




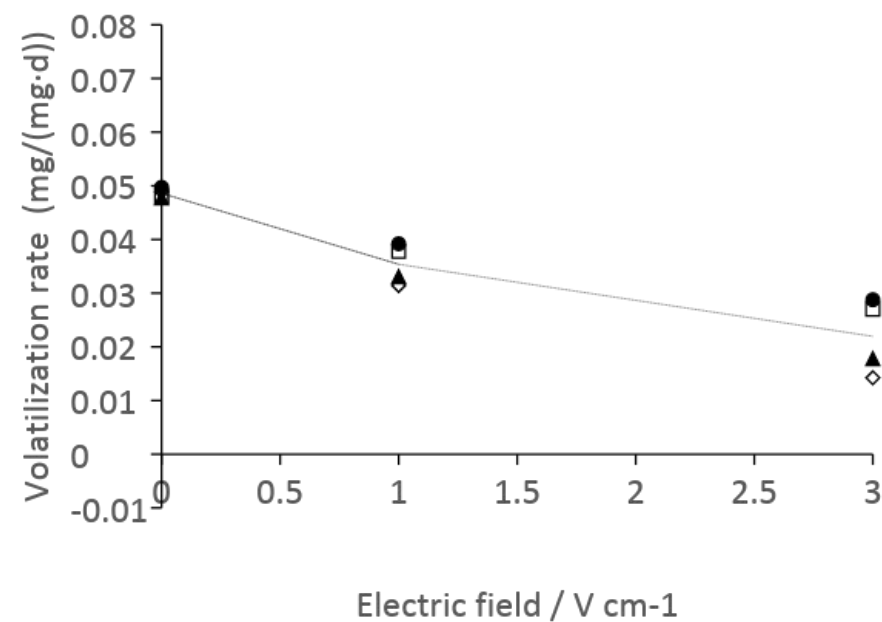
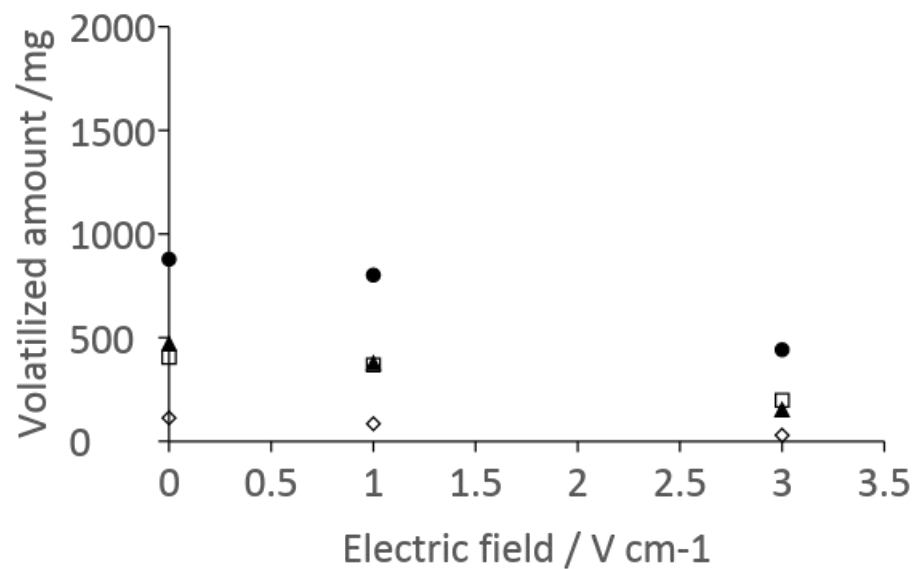
$$\frac{\partial C_i(x,t)}{\partial t} = D_{eff} \frac{\partial^2 C_i(x,t)}{\partial x^2} - u_{eff} \frac{\partial C_i(x,t)}{\partial x} - \lambda A C_i(x,t)$$



□ α -HCH ◇ ϵ -HCH ▲ δ -HCH ● γ -HCH.

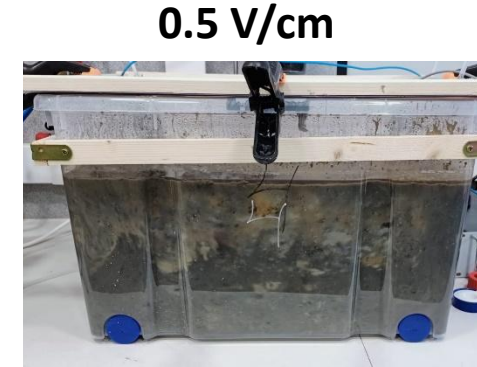
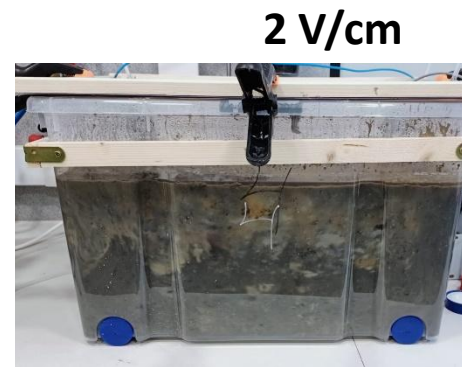


$$\frac{\partial C_i(x,t)}{\partial t} = D_{eff} \frac{\partial^2 C_i(x,t)}{\partial x^2} - u_{eff} \frac{\partial C_i(x,t)}{\partial x} - \lambda A C_i(x,t)$$

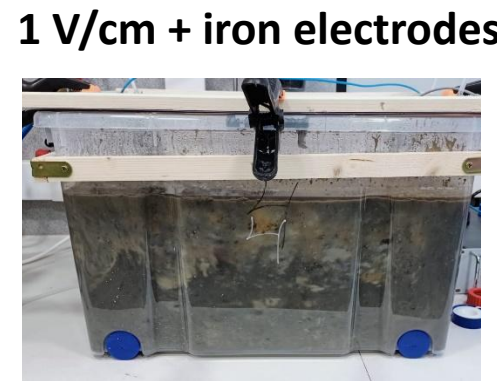
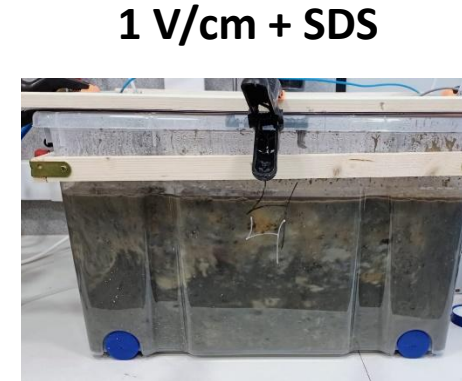
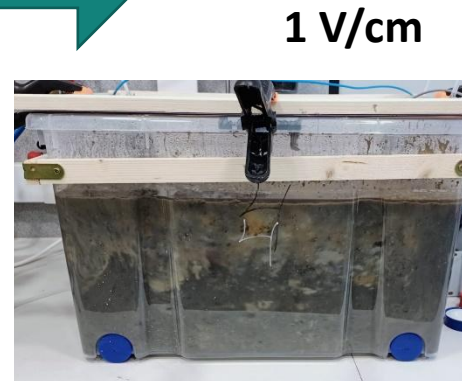


□ α-HCH ◇ ε-HCH ▲ δ-HCH ● γ-HCH.

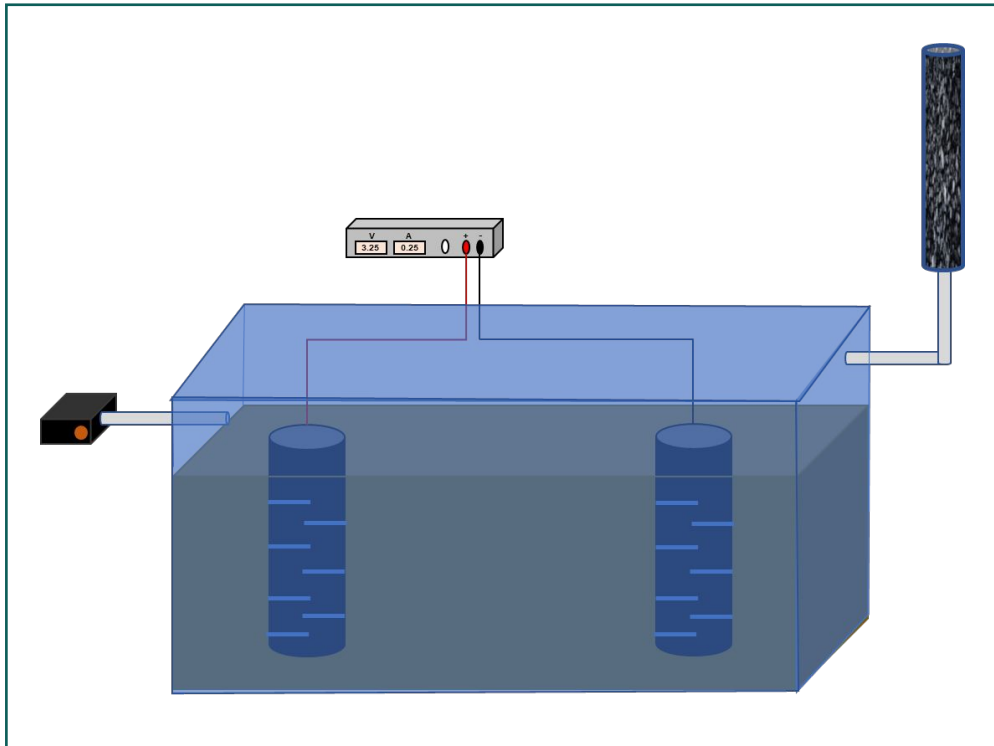
Characterization of sludge water and contaminant mobility under the action of the electric field during the first electrochemically assisted stage. Stage 2.



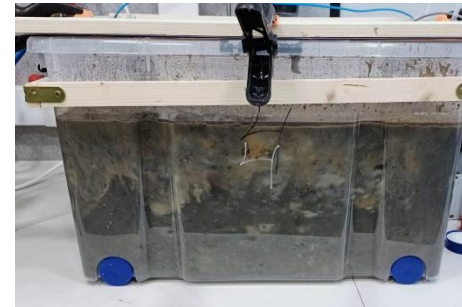
50 kg sludge / test



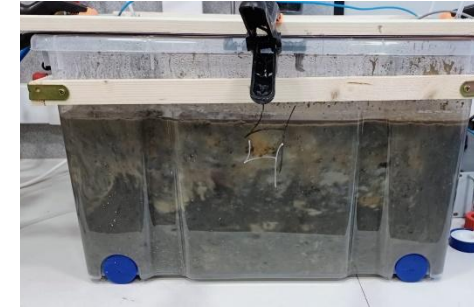
Characterization of sludge water and contaminant mobility under the action of the electric field during the first electrochemically assisted stage. Stage 2.



2 V/cm

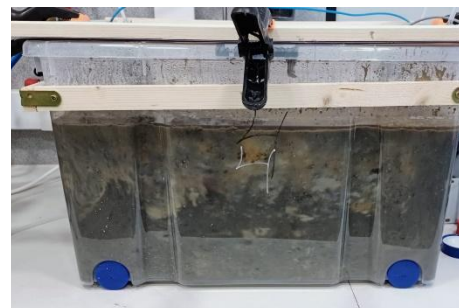


0.5 V/cm

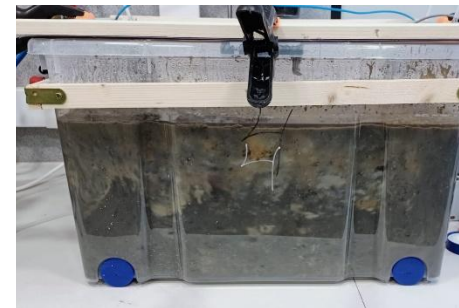


50 kg sludge / test

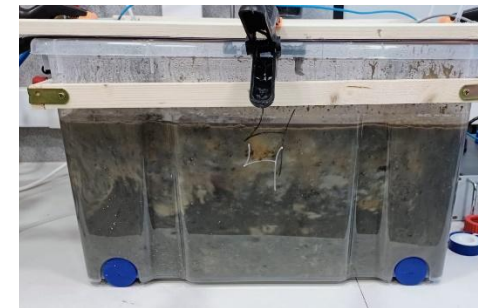
1 V/cm



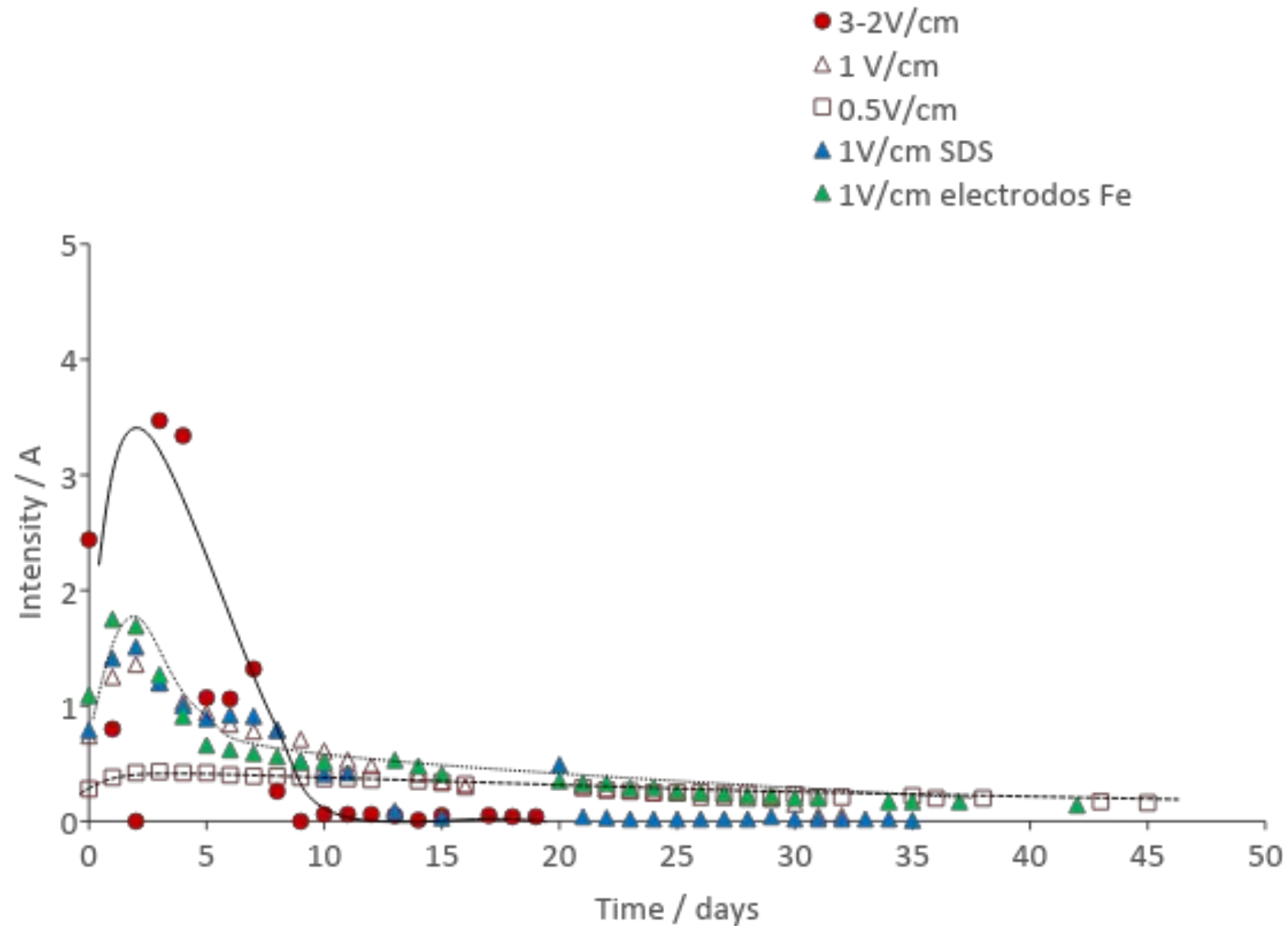
1 V/cm + SDS



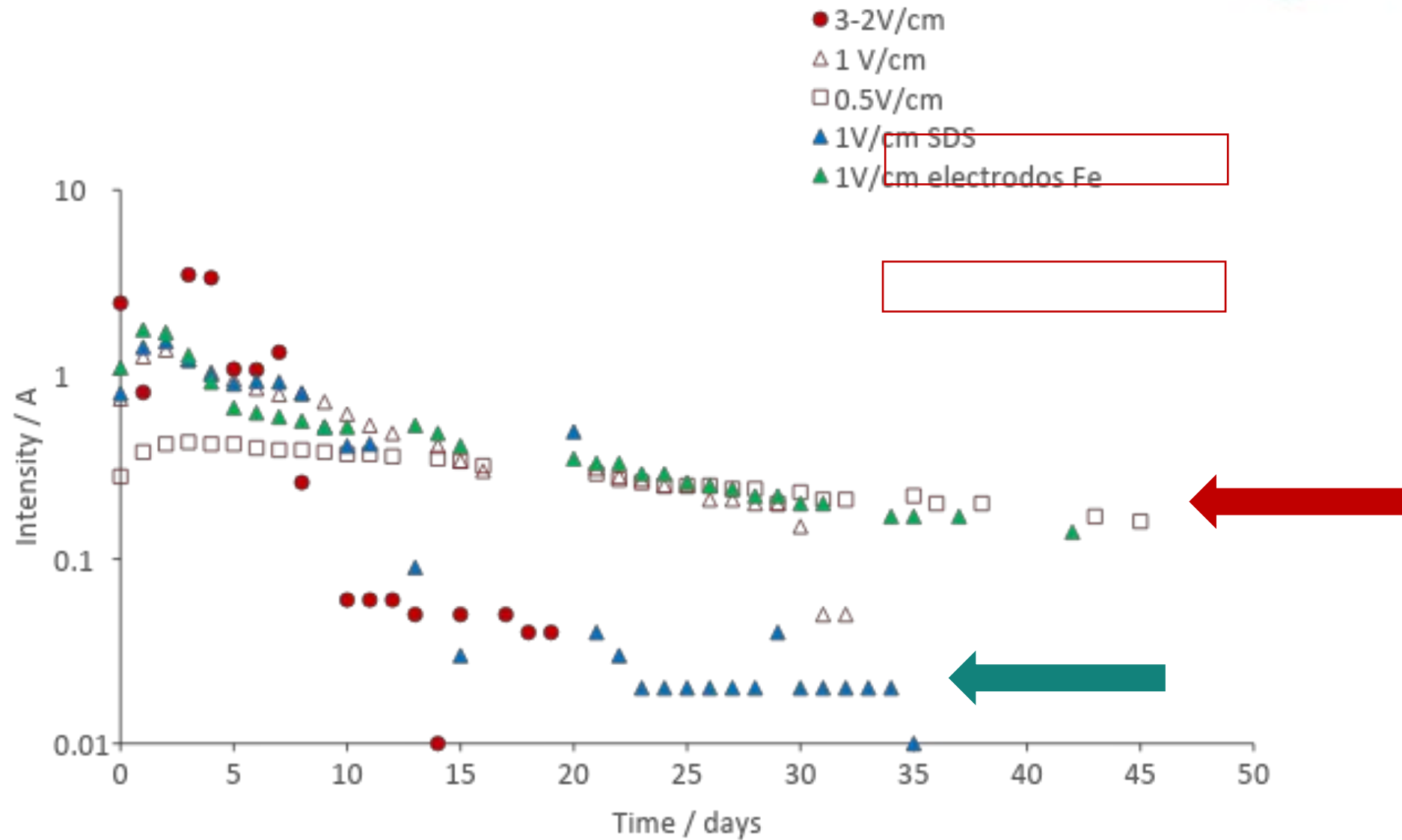
1 V/cm + iron electrodes



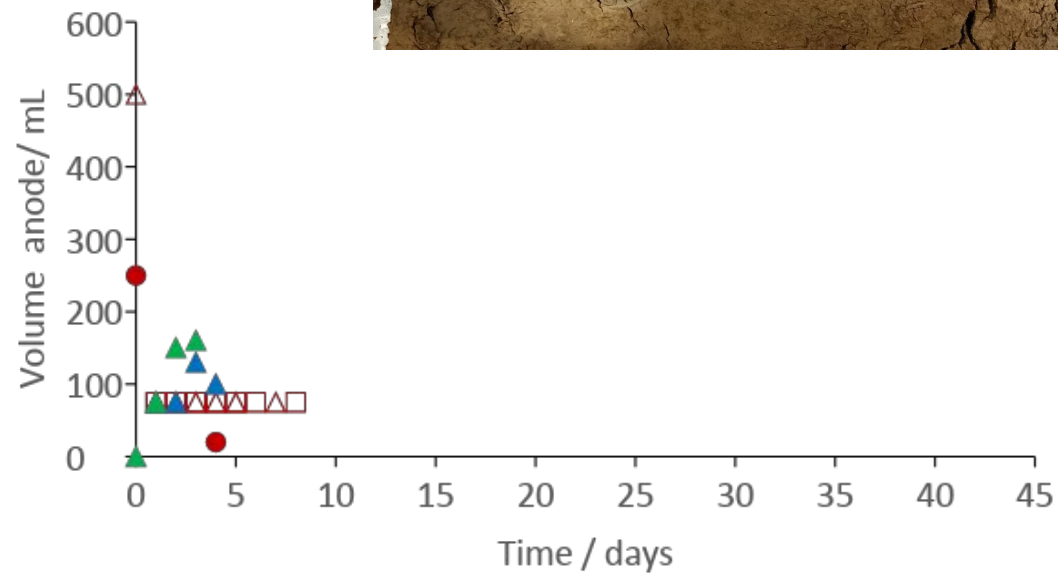
General behaviour. Current intensity.



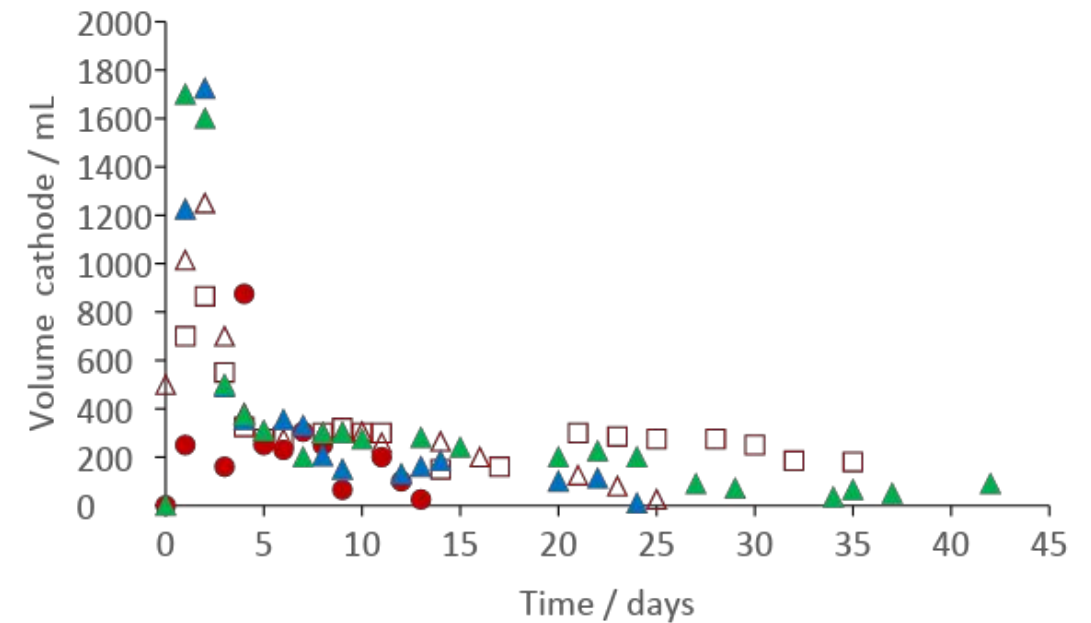
General behaviour. Current intensity.



General behaviour. Transport of water.

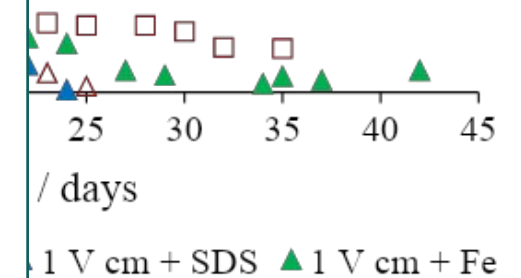
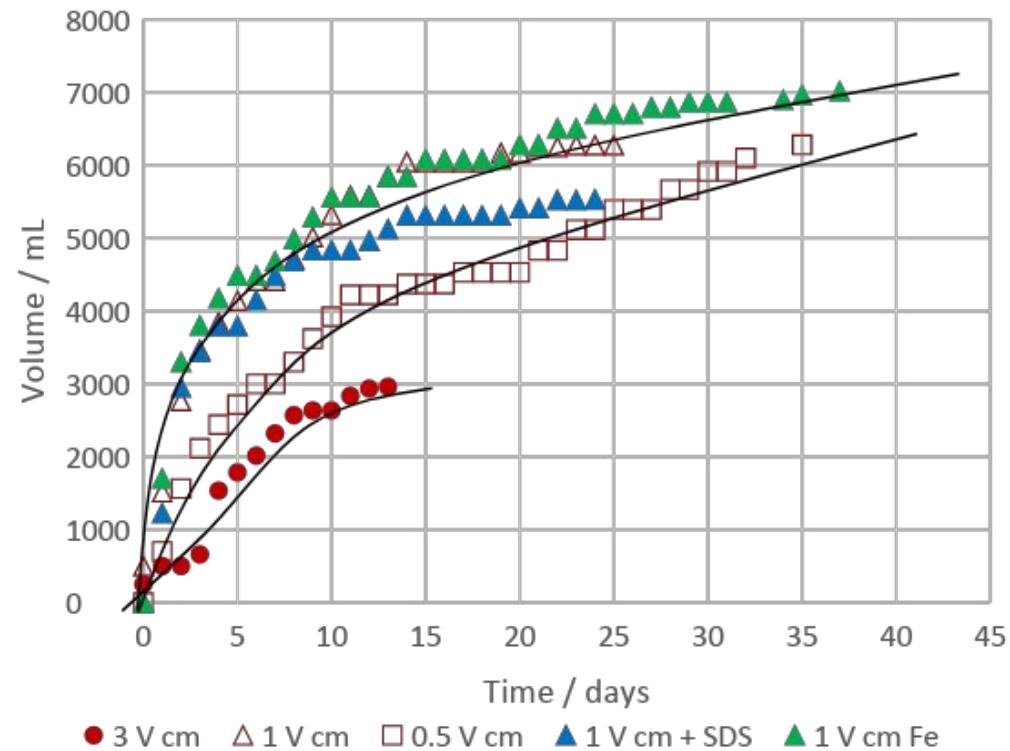
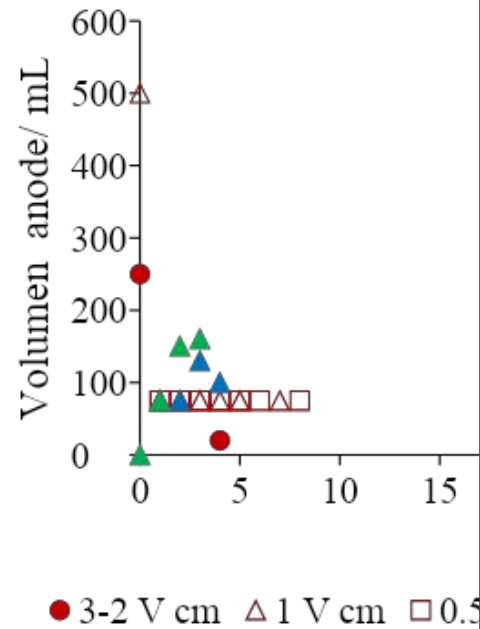


● 3-2 V cm △ 1 V cm □ 0.5 V cm ▲ 1 V cm + SDS ▲ 1 V cm + Fe

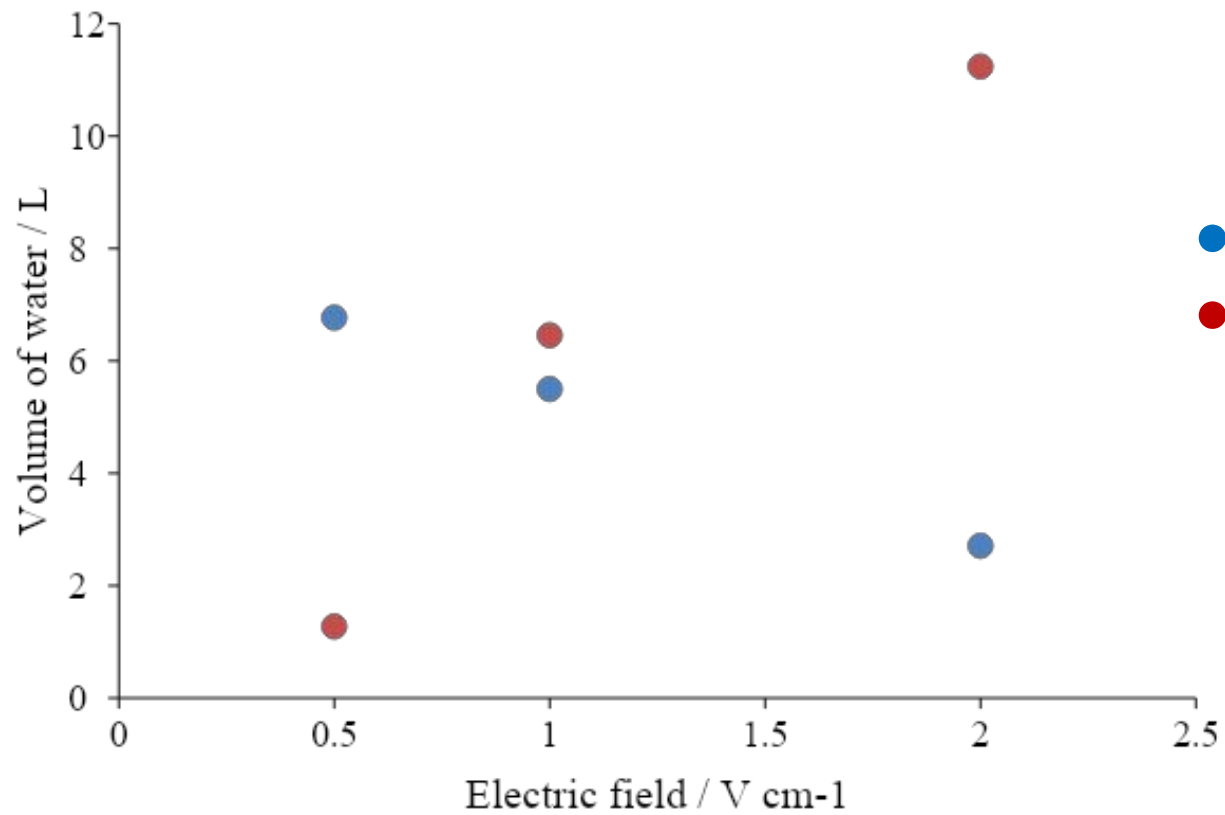


● 3-2 V cm △ 1 V cm □ 0.5 V cm ▲ 1 V cm + SDS ▲ 1 V cm + Fe

General behaviour. Transport of water.



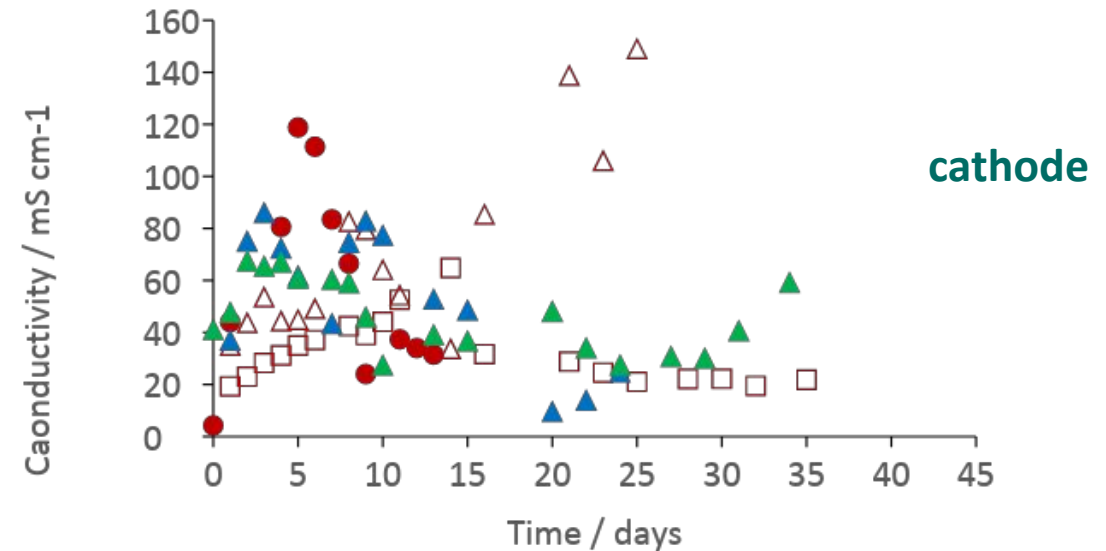
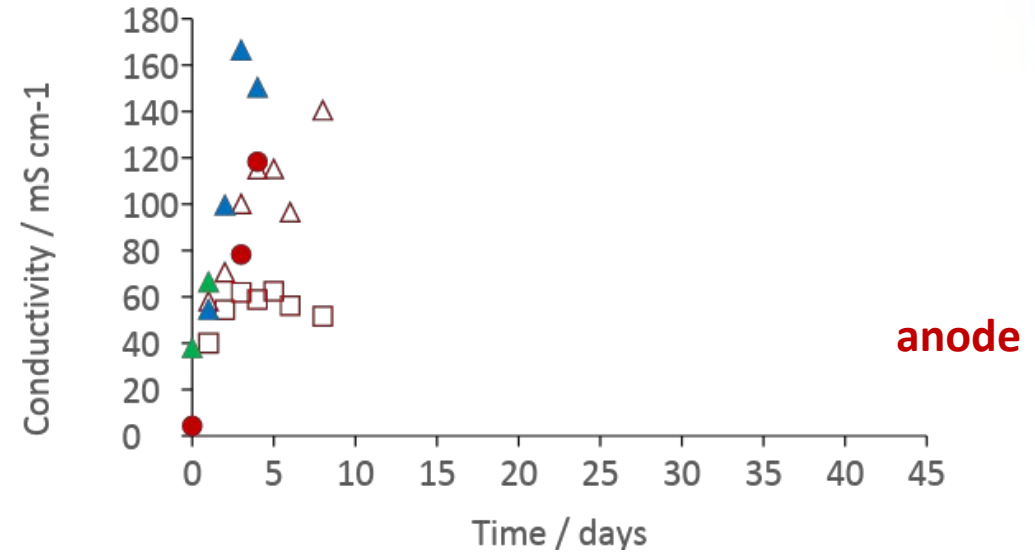
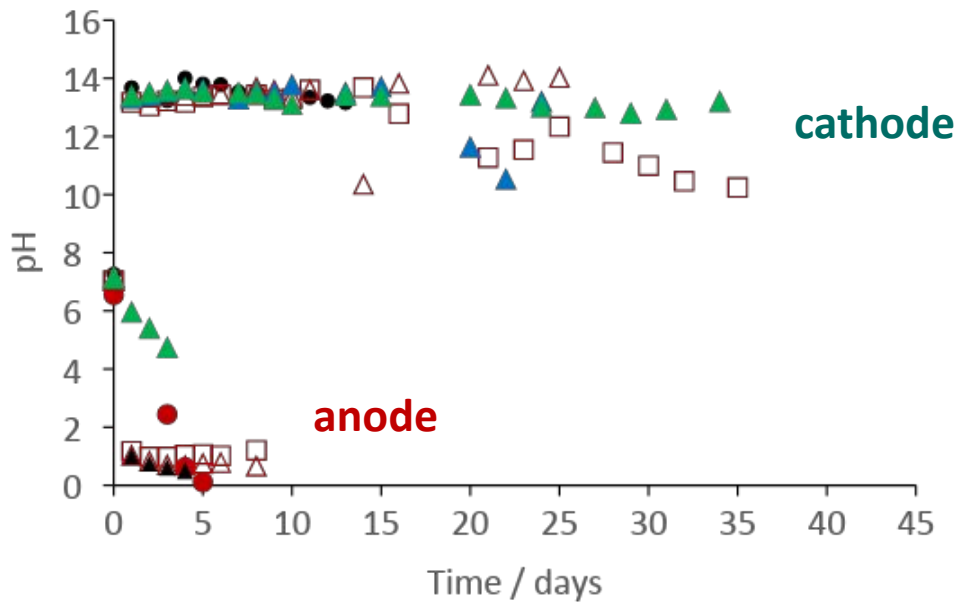
General behaviour. Transport of water.



- mobilized by EK
- evaporated

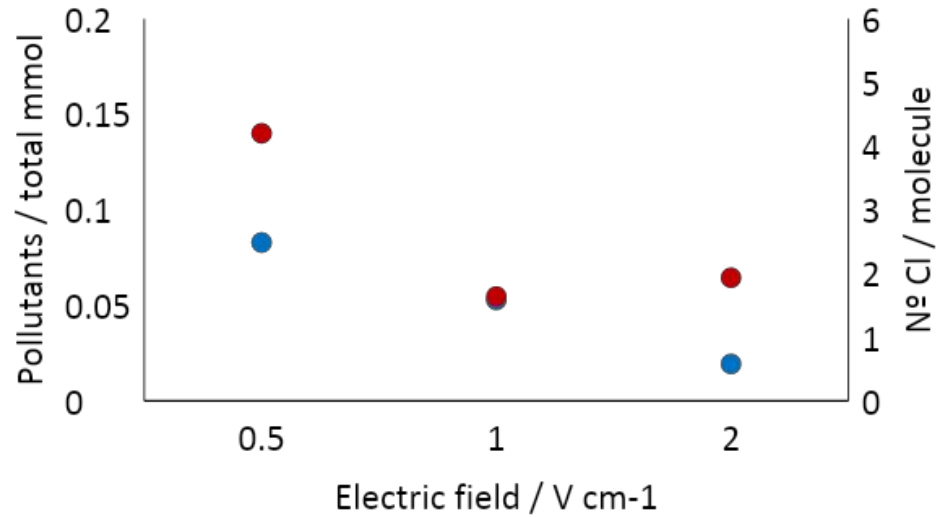


General behaviour. pH and conductivity of mobilized water.

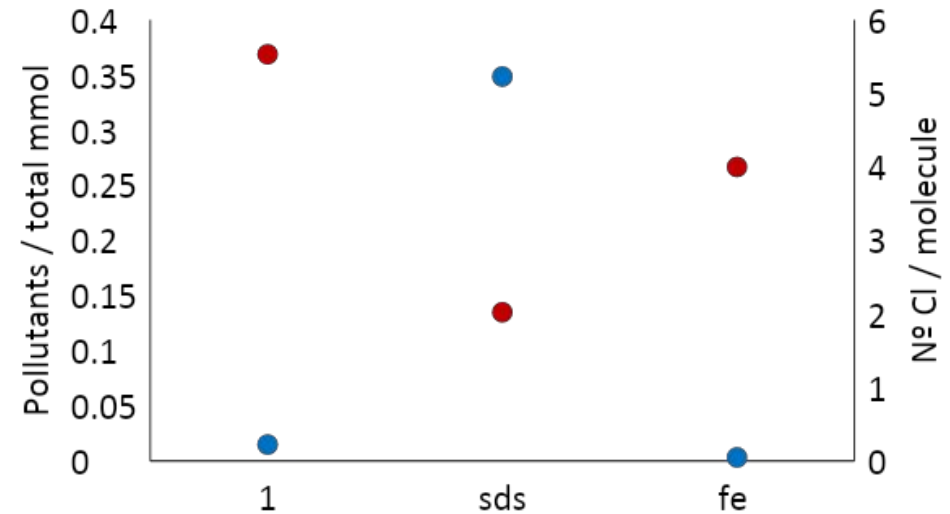
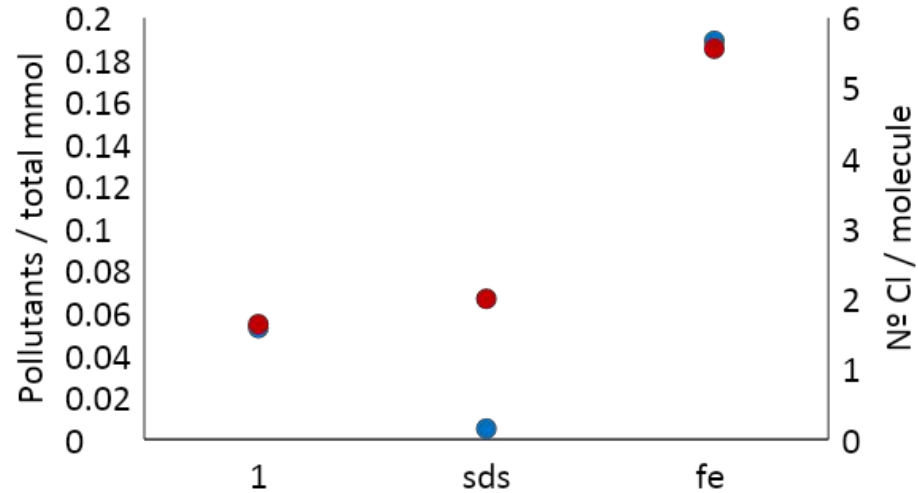
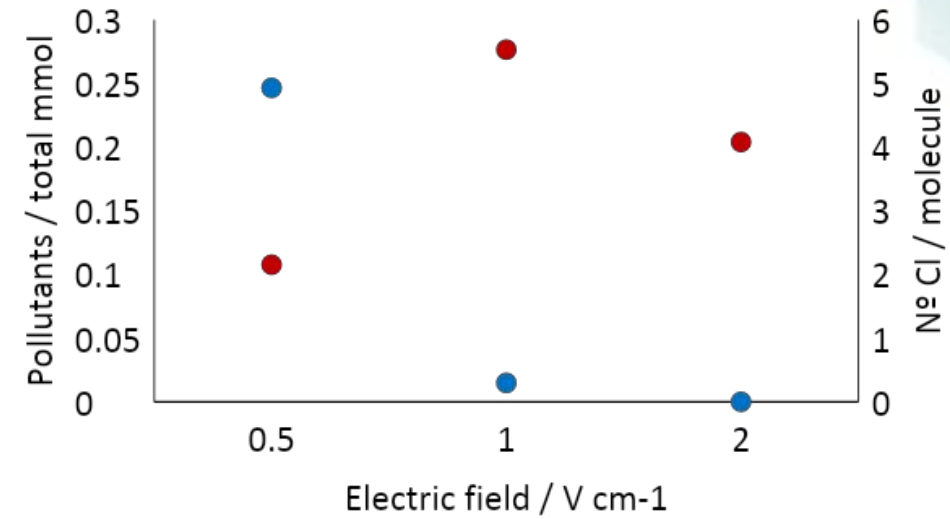


General behaviour. Organics mobilized with water.

cathode

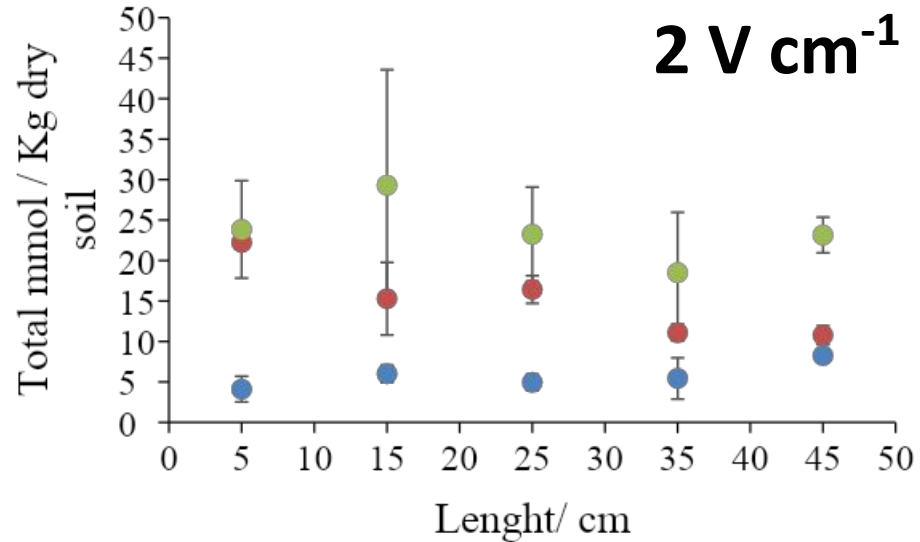


anode

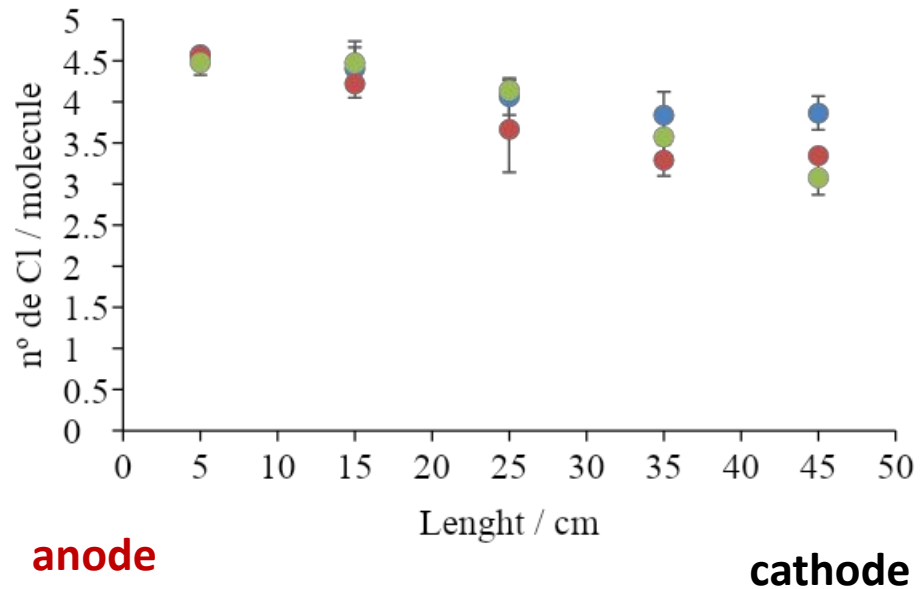


General behaviour. Organics in treated sludge.

2 V cm⁻¹



Average zone 1= 5.75 mmol / Kg SS
Average zone 2= 15.16 mmol / Kg SS
Average zone 3= 23.61 mmol / Kg SS



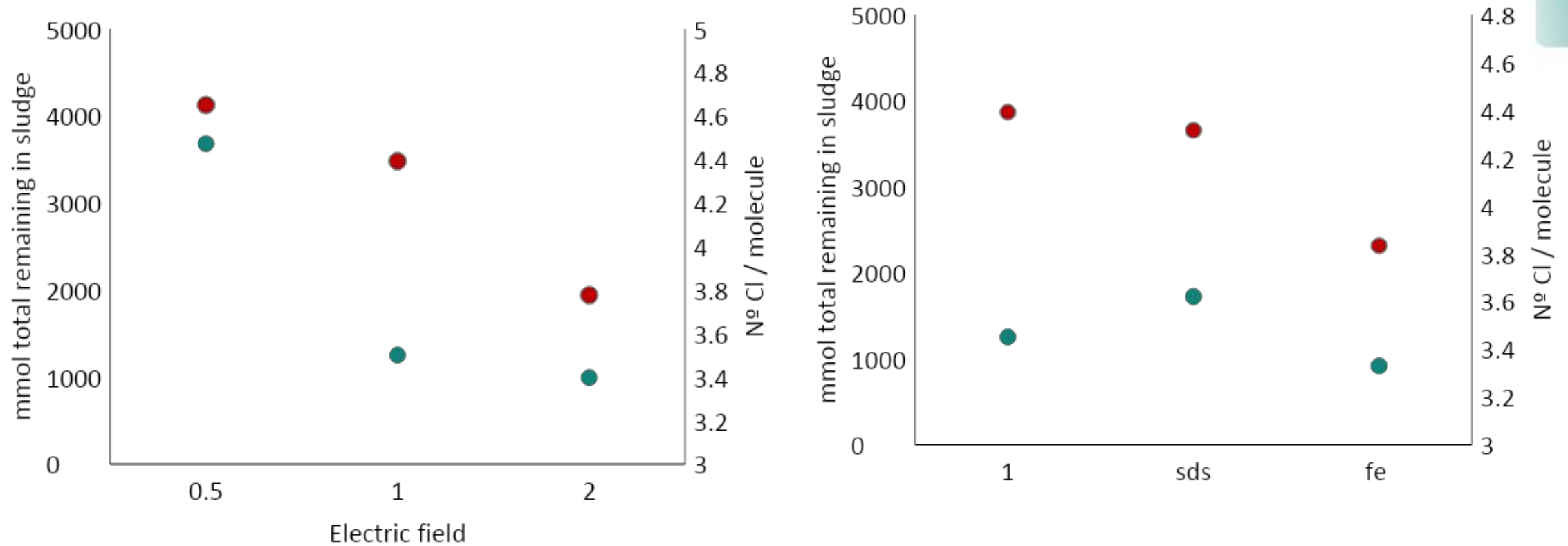
Initial average value = 4.68
Final average value=3.78

Postmortem analysis of sludge

					Zone 1
					Zone 2
					Zone 3

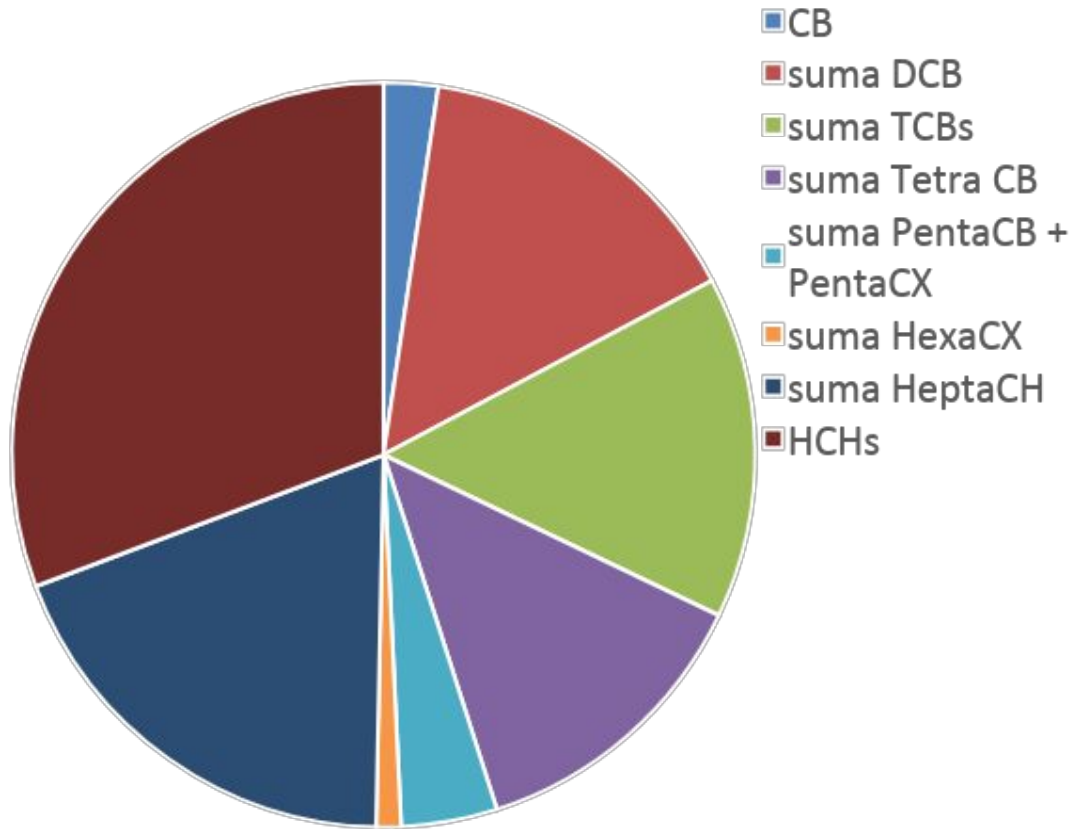
General behaviour. Organics in treated sludge.

Postmortem analysis of sludge

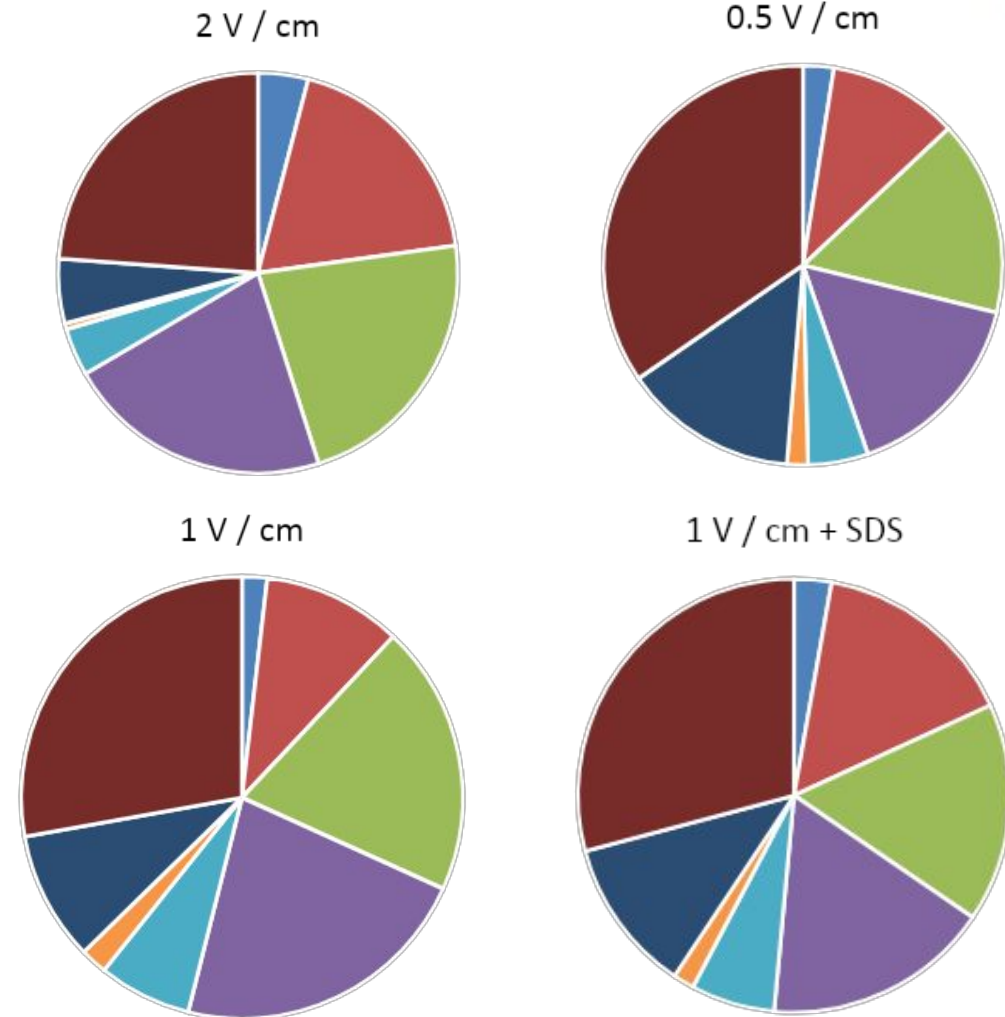


General behaviour. Organics in treated sludge.

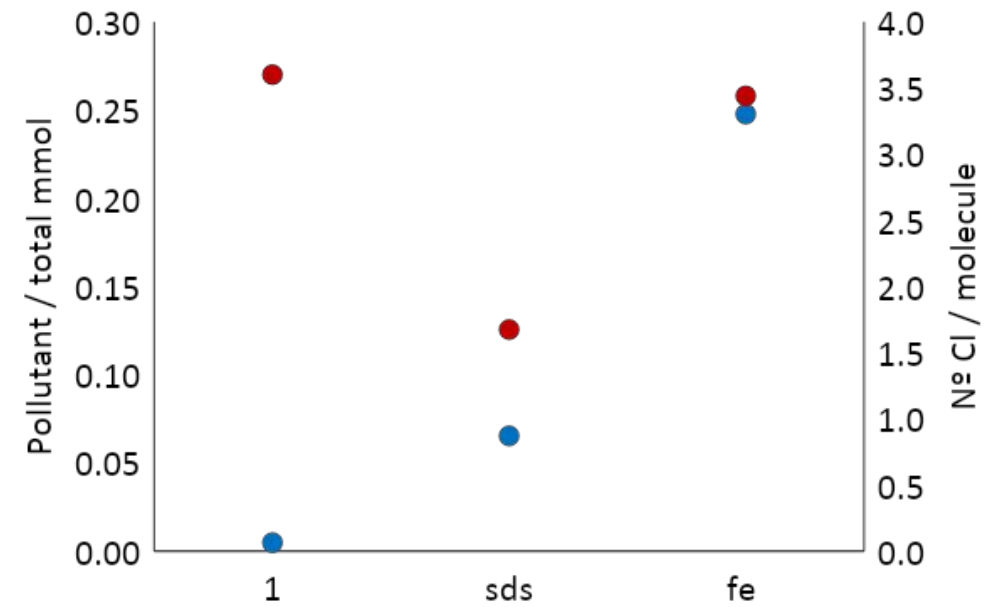
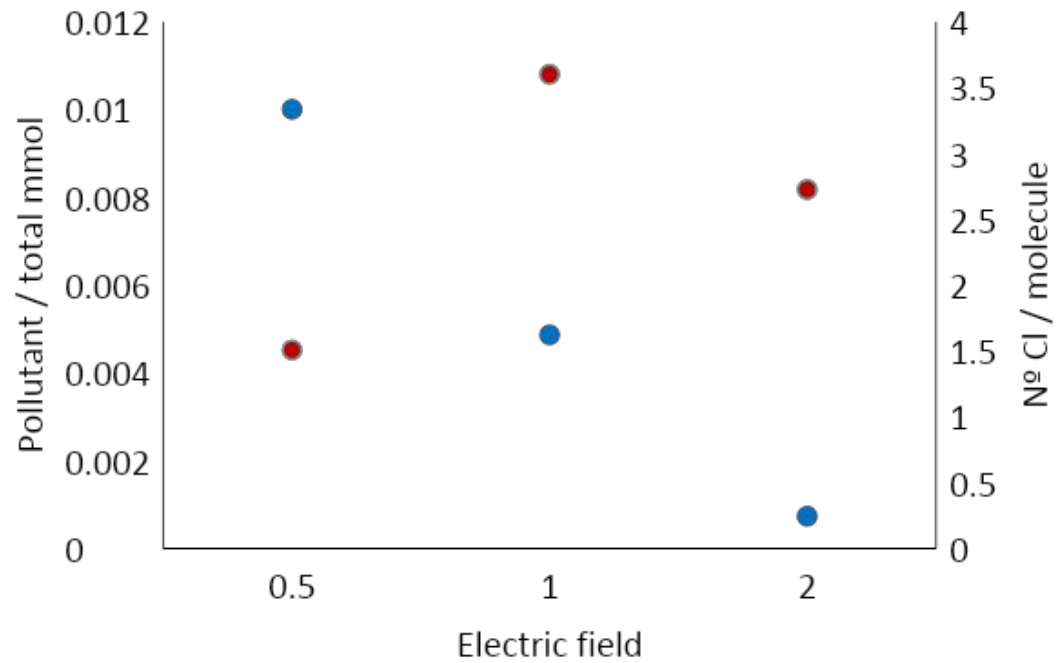
Initial pollutant distribution



Final pollutant distribution



General behaviour. Organics retained in activated carbon.



Expected results

Dragging of pollutants with electroosmotic flux

Mobilization of water by EK

Evaporation of water favoured at high cell voltage

SDS helps to drag HCH

Iron electrodes has positive effect

COVs can be transfered to gas phase

Conclusions

Pollutants are strongly retained in sludge. Low mobilization

Mobilization of water by EK, but high cell voltage leads to lower EO fluxes

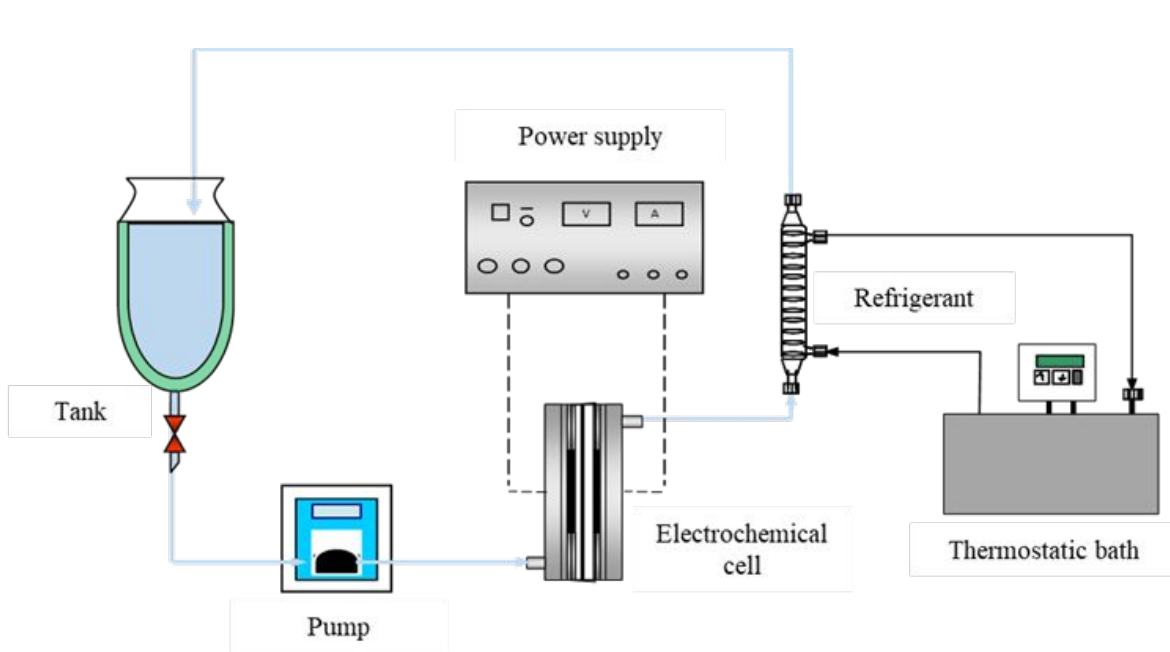
Evaporation of water is favoured at high cell voltage

Negative effect of SDS

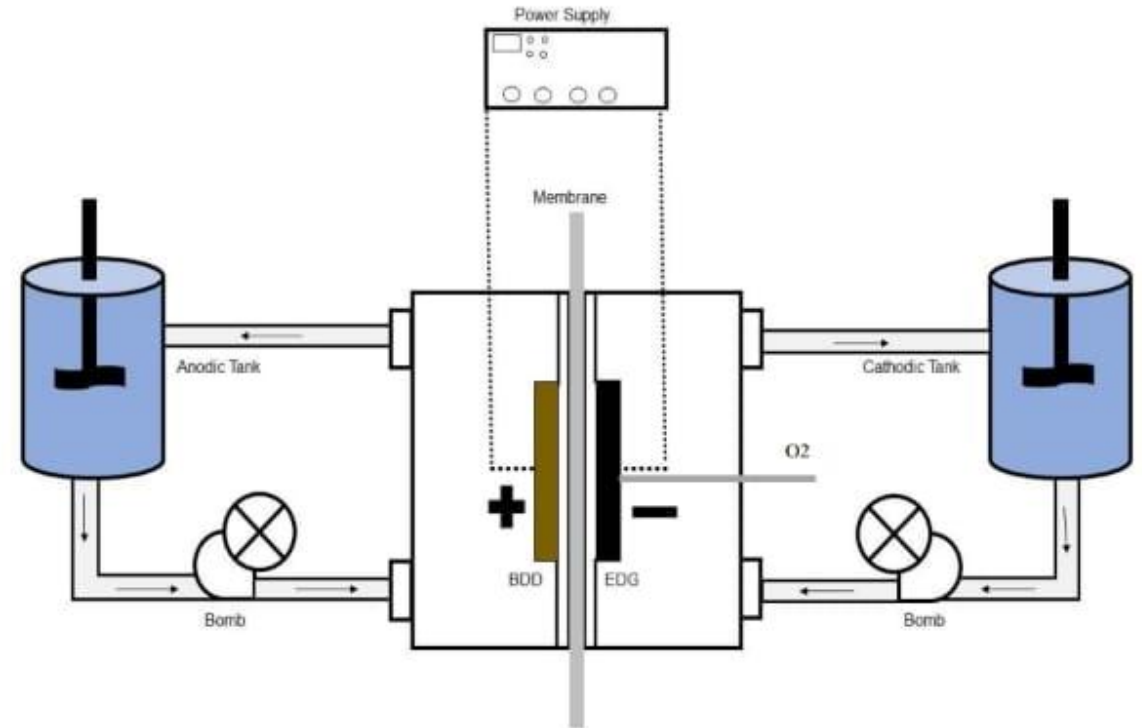
Iron electrodes contribute to minimize acid front and dehalogenation

COVs are stripped and they can be retained in GAC, but water trap should be implemented

Electrochemical treatment of extracted water.



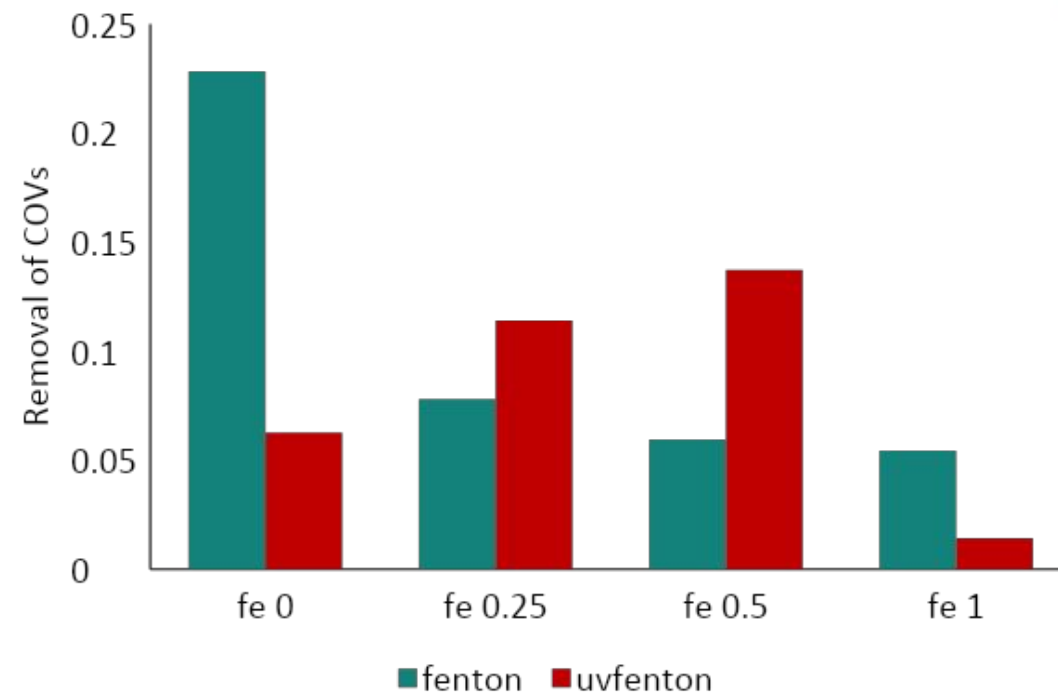
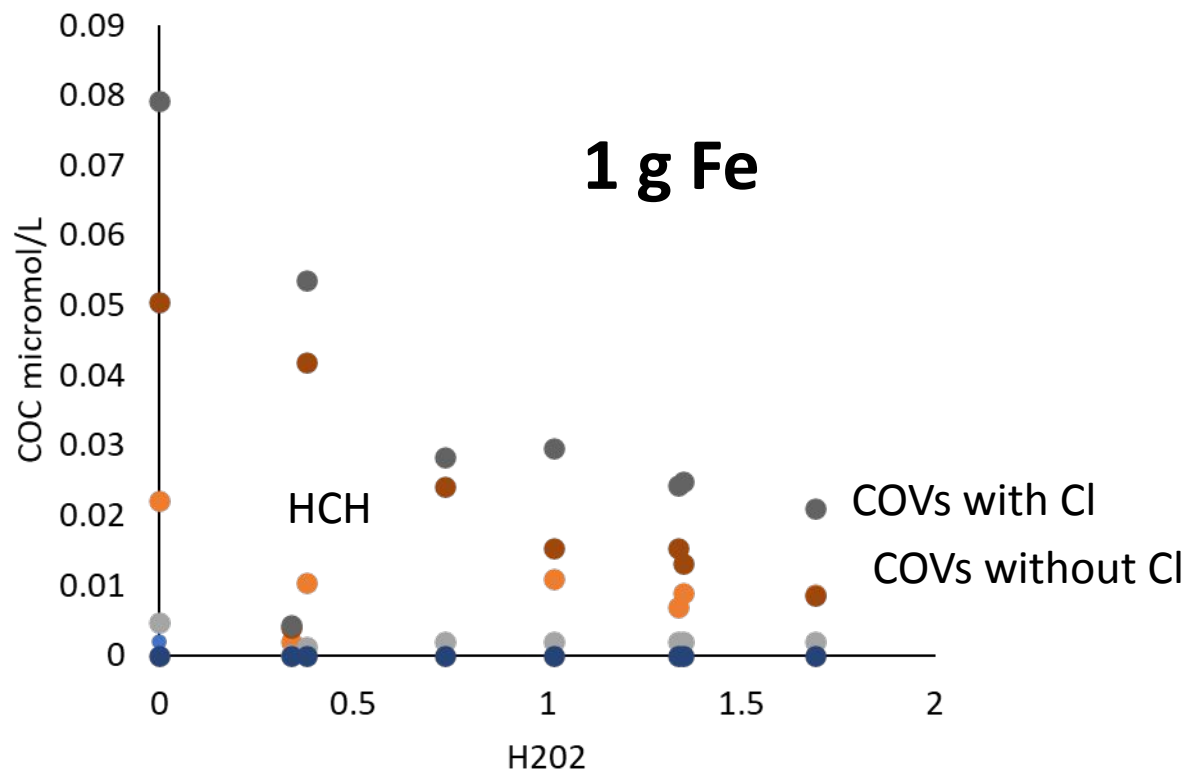
Electrolysis
PhotoElectrolysis
Electrodes: BDD and MMO



Electrofenton
Photoelectrofenton
H₂O₂/Fe ratio

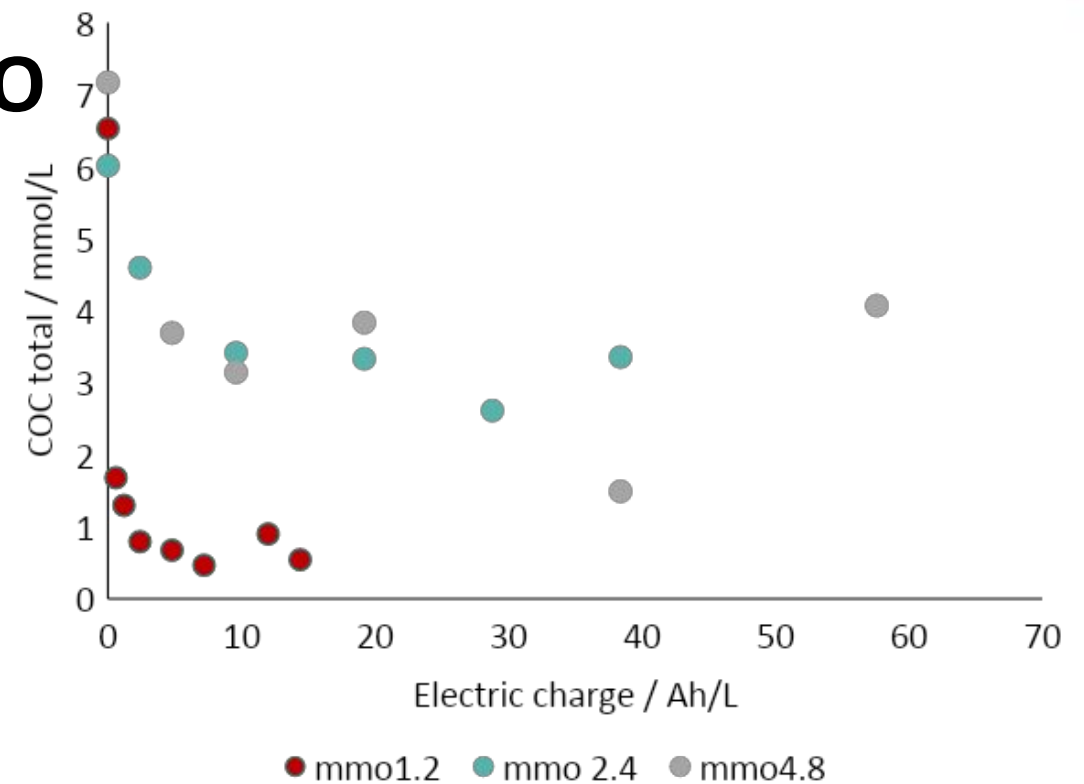
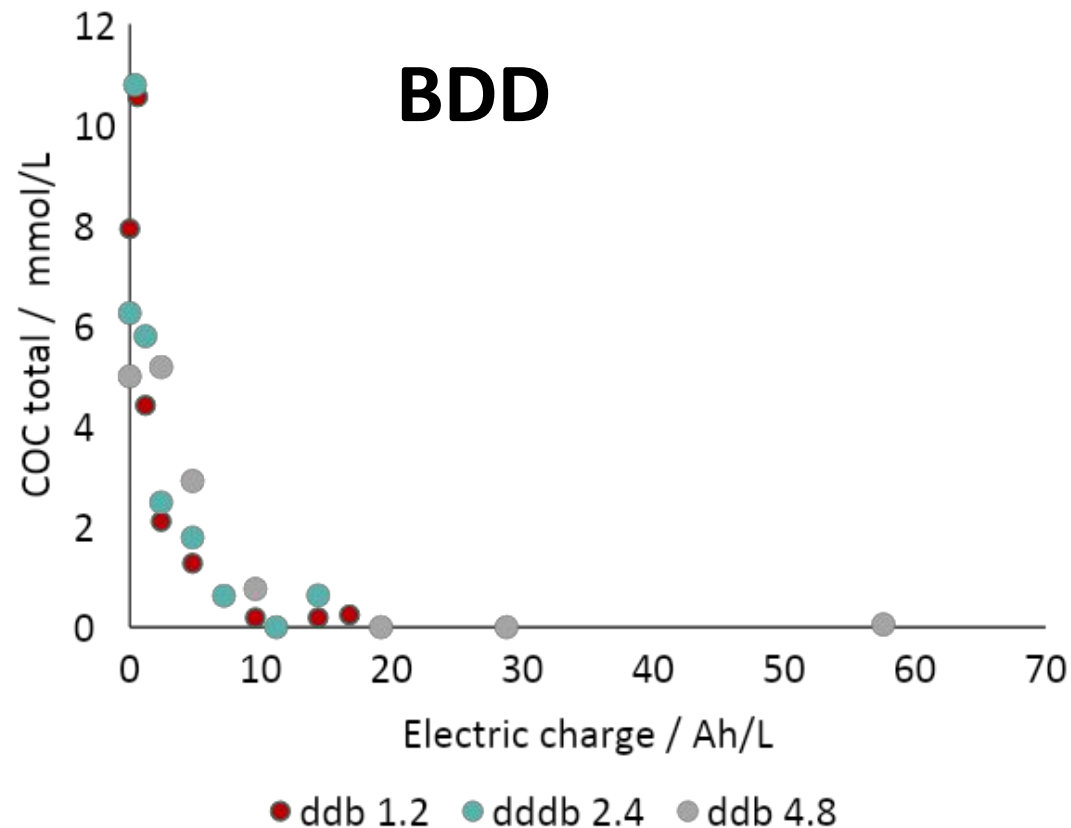
Electrochemical treatment of extracted water.

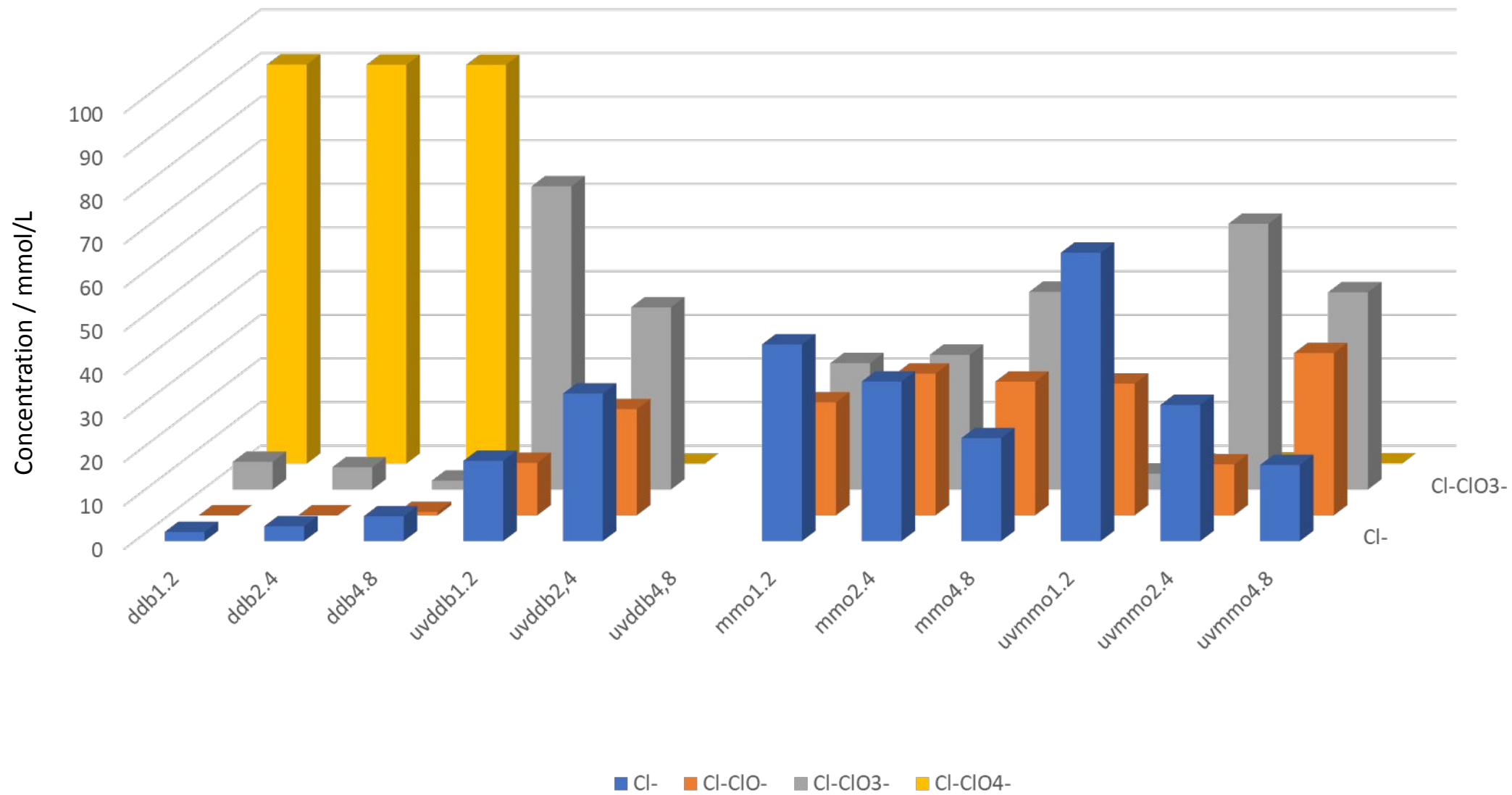
Electrofenton
Photoelectrofenton
H₂O₂/Fe ratio



Electrochemical treatment of extracted water.

Electrolysis
PhotoElectrolysis
Electrodes: BDD and MMO





Conclusions

Low efficiency of E-fenton Process.

H₂O₂ can partially degrade HCH

Electrooxidation with BDD is able to attain complete removal of HCH and derivatives, but perchlorate is also generated

Low efficiency of MMO electrodes

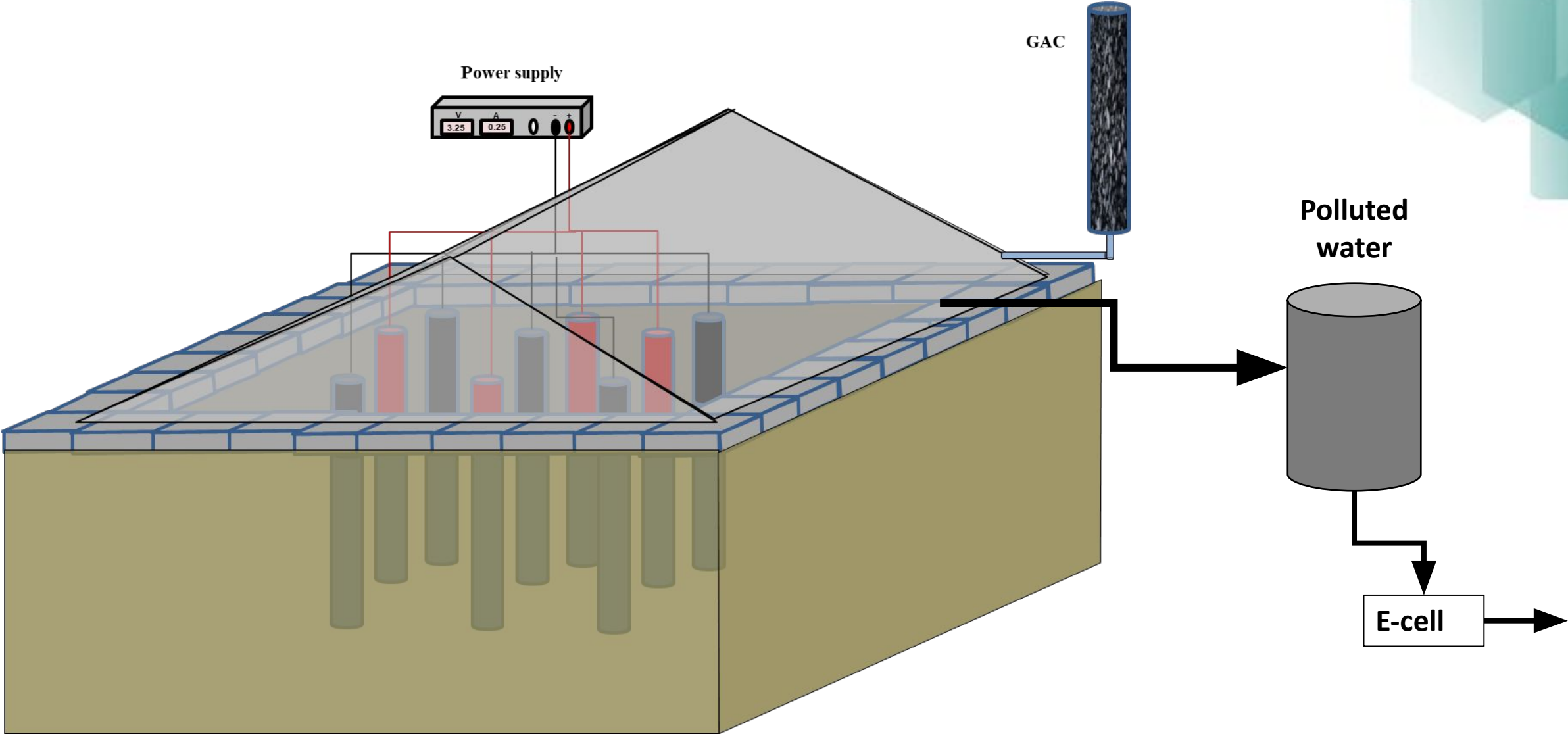
UV irradiation negatively affects COVs degradation

Direct process instead of radicalary process

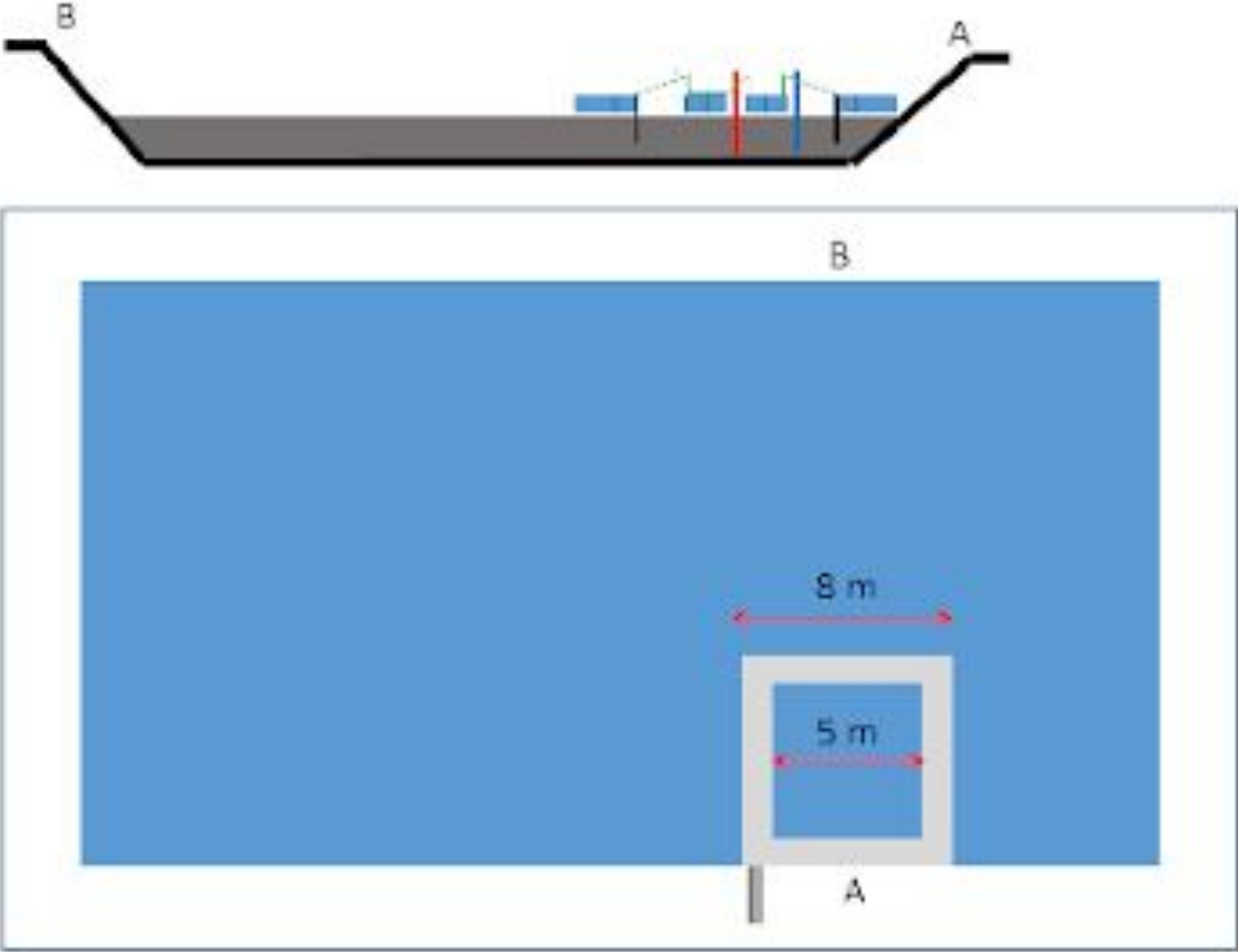


**Dismantling
sludge dump**

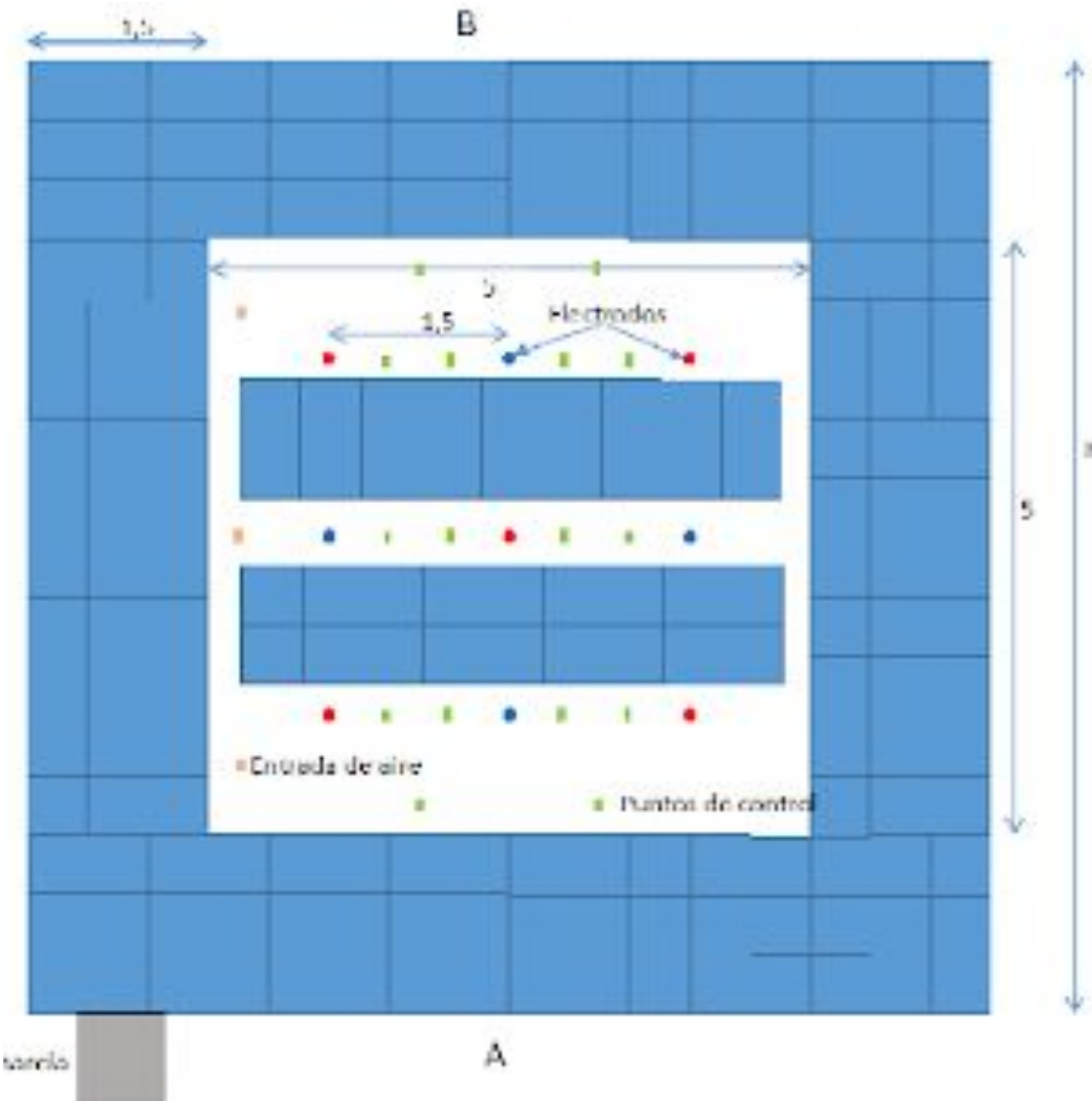
Sludge dump dismantling.



Sludge dump dismantling.



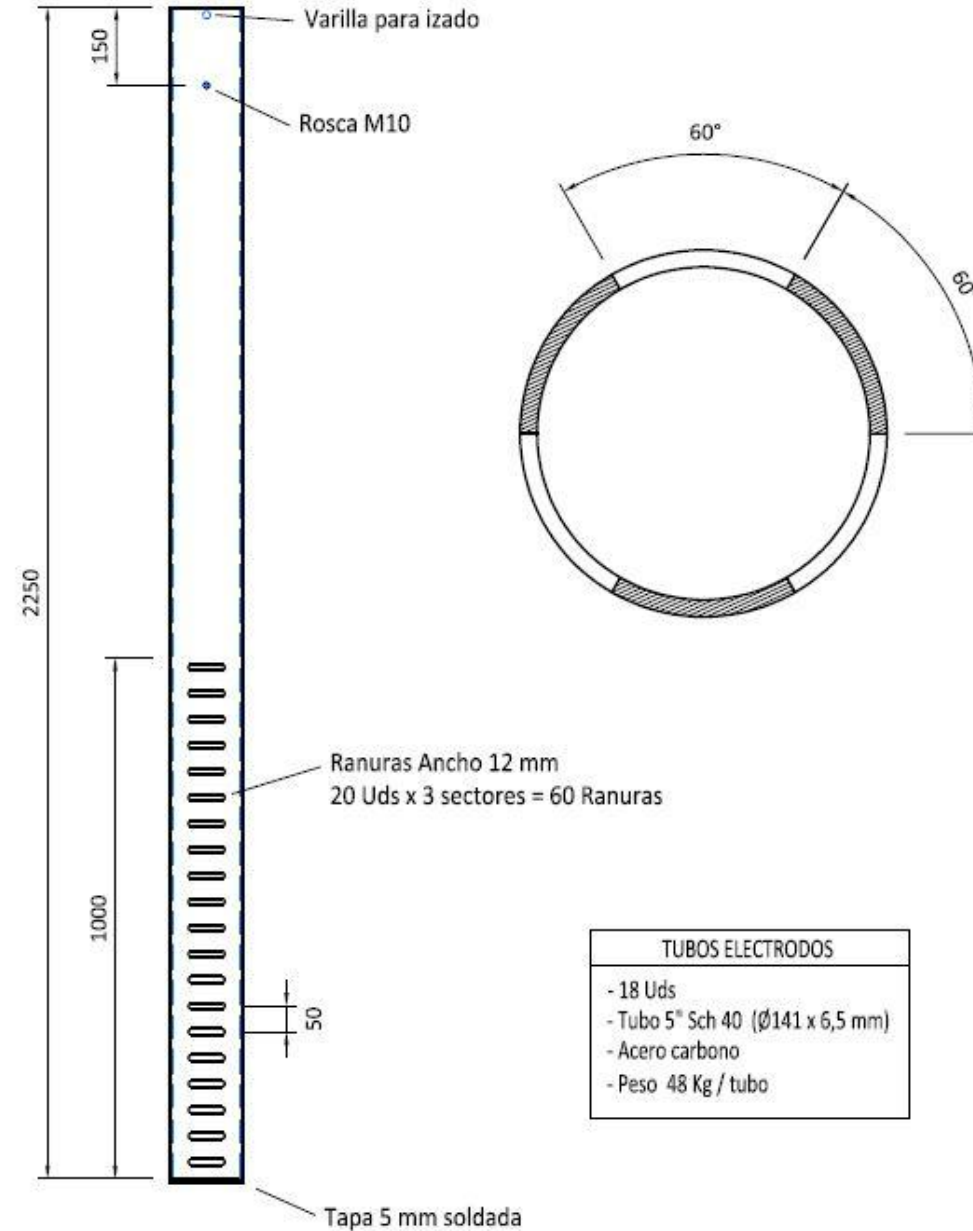
Sludge dump dismantling.



Sludge dump dismantling.

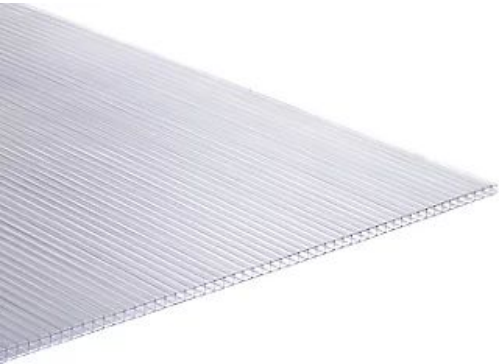
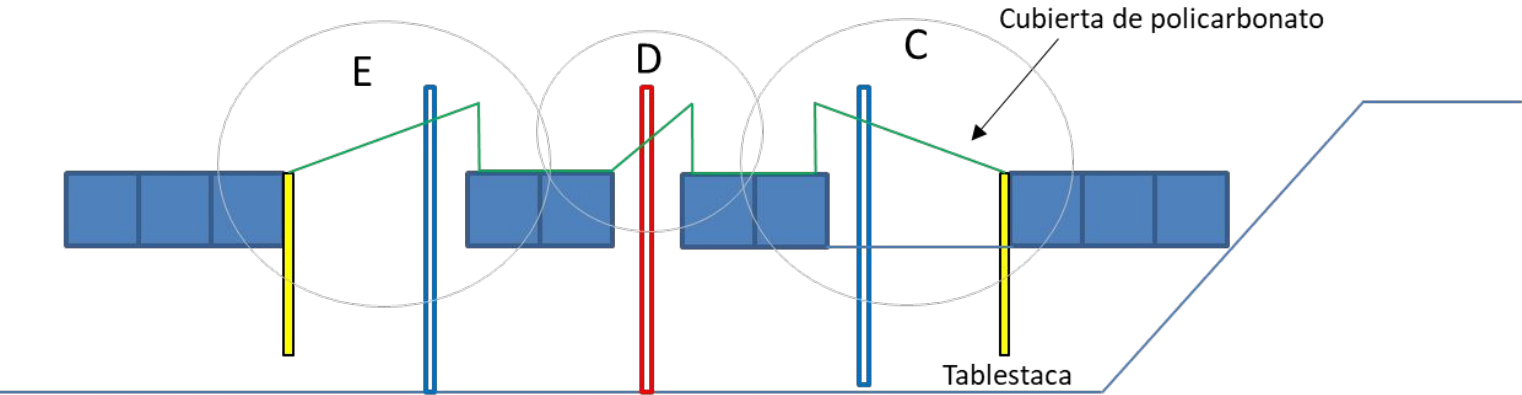
Electrodes:

Iron
hollow and perforated tube



Sludge dump dismantling.

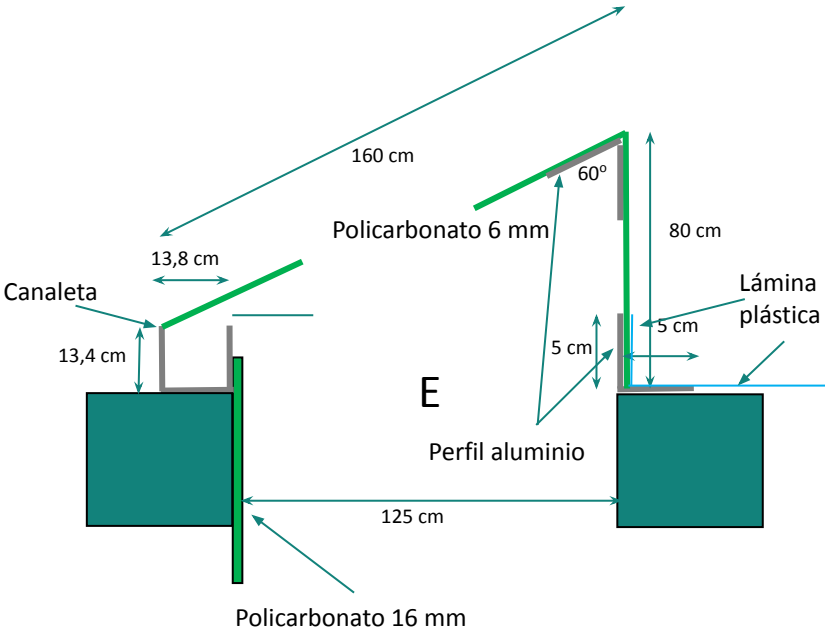
Cover:



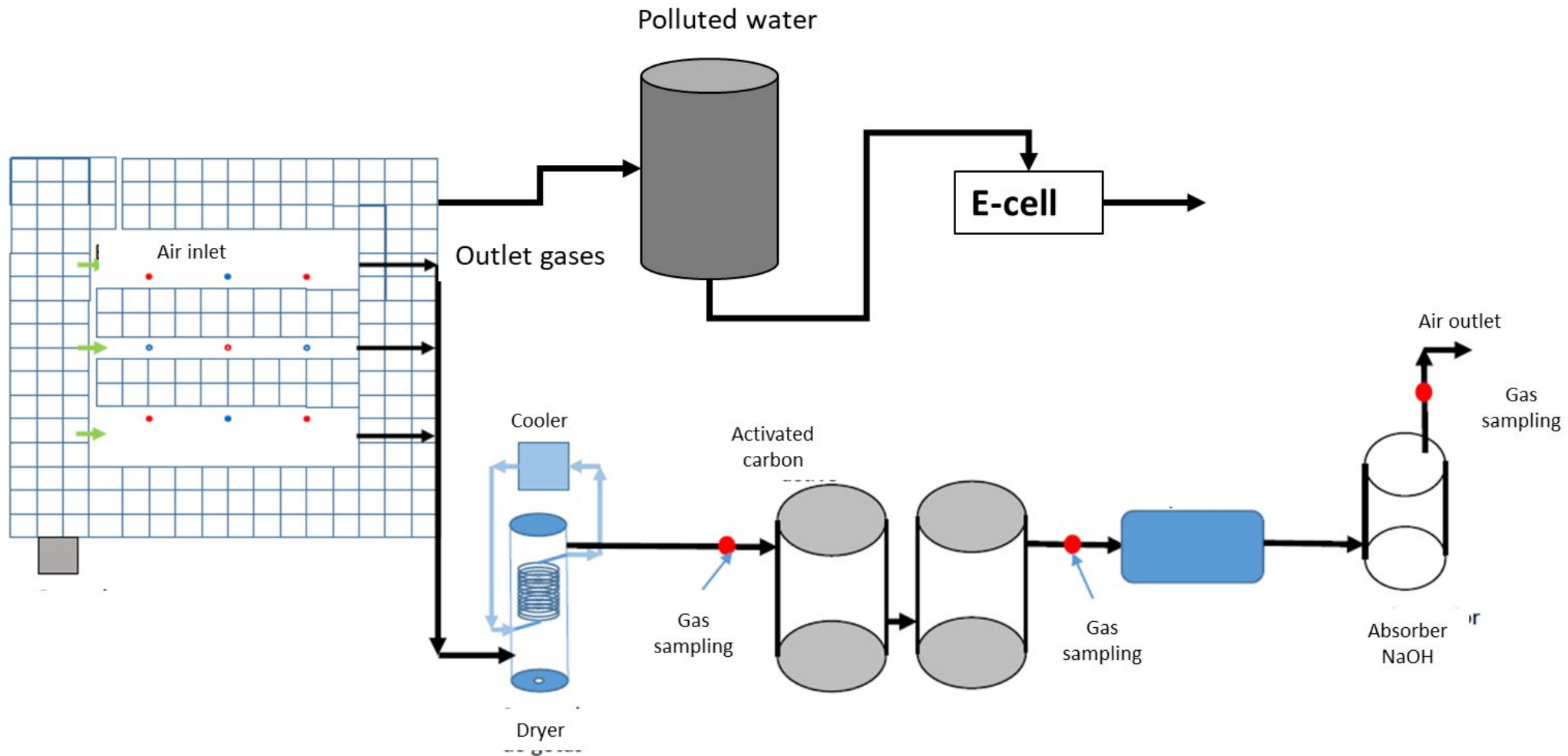
Polycarbonate plate (to cover)



Water collection channel



Sludge dump dismantling.





To be continued

THANK YOU FOR YOUR ATTENTION

Cristina.saez@uclm.es





14th
International
HCH and Pesticides
Forum